

# ASSESSMENT OF AMMONIA VOLATILIZATION FROM FLOODED SOIL SYSTEMS

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## I. INTRODUCTION

Ammonia volatilization from flooded soil systems involves a complex pathway in the terrestrial-atmospheric nitrogen (N) cycle. Ammonium N derived from natural sources (fertilized rice paddies and industrial by-products, lakes, streams, ponds, animal wastes, etc.) are potential materials for  $\text{NH}_3$  volatilization. In recent years, losses of soil N fertility via volatilization have been identified as a major constraint to crop production, both with upland and lowland crops, particularly rice grown on flooded soils. In flooded rice culture, where ammonium ( $\text{NH}_4^+\text{-N}$ ) fertilizers are broadcast directly onto the soil or water without incorporation,

NH<sub>3</sub> volatilization losses range from 10 to 60% of the fertilizer N applied. In contrast, where the fertilizer N is placed in the soil (e.g., 10 cm deep) by either mixing, placement, or banding techniques, NH<sub>3</sub> losses may be very minimal (<5%). Poor fertilizer management practices may contribute significantly to low fertilizer-use efficiency with resultant poor crop yields.

A variety of water, soil, biological, and environmental factors and management practices influence the kinetics and extent of NH<sub>3</sub> volatilization from flooded soil systems. Ammoniacal N concentration, pH, P<sub>CO<sub>2</sub></sub>, alkalinity, buffering capacity, temperature, depth, turbulence, and biotic activity are several floodwater characteristics that influence NH<sub>3</sub> volatilization. The NH<sub>4</sub><sup>+</sup>-N concentration in floodwater is influenced by N management practices such as source, timing and method of application, and water depth as well as biotic activity.

The dominant soil factors affecting NH<sub>3</sub> volatilization are soil pH, redox status, cation exchange characteristics, CaCO<sub>3</sub> content, soil texture, biotic activity, and fluxes affecting adsorption and desorption of NH<sub>4</sub><sup>+</sup>-N at the soil–water interface. Atmospheric conditions such as windspeed, P<sub>NH<sub>3</sub></sub>, air temperature and solar radiation also influence NH<sub>3</sub> volatilization. Management practices concerning the crop, water, and soil together with weather conditions prior to and after crop establishment have a direct effect on NH<sub>3</sub> losses.

Problems of measuring NH<sub>3</sub> volatilization losses to accurately reflect dynamic field conditions have long been a concern of researchers and planners. Methods used to measure NH<sub>3</sub> loss have been described by Fillery and Vlek (1986) and also by Harper (1988) who identify the problems associated with quantifying losses under undisturbed field conditions. They describe three micrometeorological methods that have promise, mainly eddy correlation, gradient diffusion, and mass balance.

The behavior of NH<sub>4</sub><sup>+</sup>-N in flooded soil systems and the mass transfer of NH<sub>3</sub> across the water–air interface is a dynamic process involving numerous interactions. An understanding of the rate-controlling factors described in a simplified model will enable us to predict losses, allow simplified measurements, and subsequently aid the planning and decision making processes in controlling NH<sub>3</sub> losses to the atmosphere from natural systems, as well as designing more efficient fertilizer management strategies.

Only a few models have been published which analyze the floodwater chemistry and atmospheric conditions affecting NH<sub>3</sub> volatilization (Bouwmeester and Vlek, 1981a; Moeller and Vlek, 1982; Jayaweera and Mikkelsen, 1990a).

Several good reviews have been published which summarize the general information on NH<sub>3</sub> volatilization in flooded soil systems (Vlek and Cras-

well, 1981; Fillery and Vlek, 1986). Readers new to the field may wish to refer to these reviews for the early research.

## II. THEORETICAL ASPECTS

Volatilization is the process by which a substance is transferred from a liquid or solid phase to a vapor phase, generally the atmosphere. Ammoniacal N occurring in a floodwater system may be transferred to the atmosphere as gaseous NH<sub>3</sub> across the water–air interface.

### A. CHEMICAL ASPECTS

The ammonium ion, NH<sub>4</sub><sup>+</sup>-N is the source of NH<sub>3</sub>, which is formed as a N-transformation product in flooded soil, and also found following N fertilizer applications. The NH<sub>4</sub><sup>+</sup>-N pool establishes an equilibrium with dissolved NH<sub>3</sub> gas, NH<sub>3(aq)</sub>, which is governed by the pH of the medium. The dissociation reaction of NH<sub>4</sub><sup>+</sup>/NH<sub>3(aq)</sub> equilibrium is of first order, whereas the association reaction is considered to be of second order (Alberty, 1983).

Volatilization of a chemical from a water body is described as a first-order process (Smith *et al.*, 1981). Several researchers have shown that NH<sub>3</sub> volatilization per se follows first-order kinetics (Folkman and Wachs, 1973; Vlek and Stumpe, 1978; Moeller and Vlek, 1982).

The reaction sequence for NH<sub>3</sub> volatilization is as follows:



where

$k_d$  = dissociation rate constant for NH<sub>4</sub><sup>+</sup>/NH<sub>3(aq)</sub> equilibrium;

$k_a$  = association rate constant for NH<sub>4</sub><sup>+</sup>/NH<sub>3(aq)</sub> equilibrium; and

$k_{vN}$  = volatilization rate constant for NH<sub>3</sub>.

### B. VOLATILIZATION ASPECTS

The transfer of NH<sub>3</sub> across a water–air interface is described by the two-film model proposed by Whitman (1923), a useful concept to describe the mass transfer of a gas across a liquid–gas interface (Coulson *et al.*, 1978). According to this model, the main body of each fluid is assumed to

be well mixed by convection currents and the concentration differences are regarded as negligible except in the vicinity of the interface between the phases. On either side of the interface it is supposed that turbulent eddies die out and that there exists a thin film of fluid in each phase, the flow of which is considered to be laminar and parallel to the surface (Fig. 1). This film, however, can also be considered as a stagnant layer on either side of the interface. Most of the resistance to mass transfer, and hence most of the concentration gradient, lies in these films. Outside this layer, turbulent eddies supplement the action caused by the random motion of the molecules, and the resistance to transfer becomes progressively smaller. The basis of the theory is the assumption that the zones in which the resistance to transfer lie can be replaced by two hypothetical layers, one on each side of the interface, in which the transfer is solely by molecu-

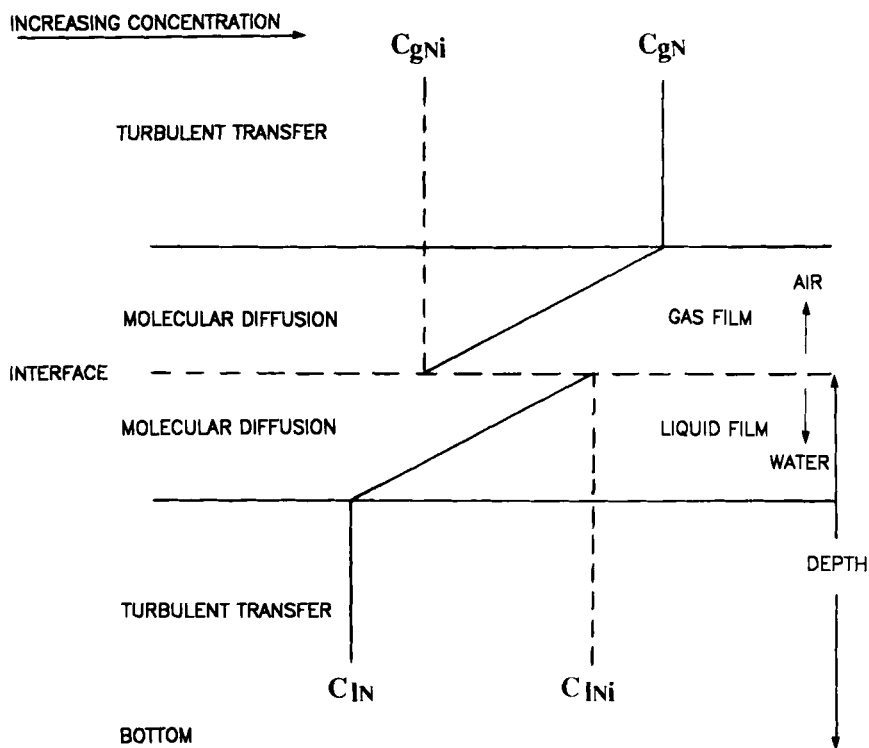


FIG. 1. Two-film model of a gas-liquid interface:  $C_{gN}$  and  $C_{lN}$ , average  $\text{NH}_3$  concentrations in bulk gas and liquid phase, respectively;  $C_{gNi}$  and  $C_{liNi}$ , average  $\text{NH}_3$  concentrations at the interface in gas and liquid phase, respectively. (Adapted from Liss and Slater, 1974).

lar diffusion. The concentration gradient is therefore linear in each of these layers and zero outside. Under given conditions of turbulence, however, the layer thicknesses vary both spatially and temporally (Liss and Slater, 1974). According to Smith and Bomberger (1979), high turbulence in the liquid causes the liquid film or boundary layer to be thin; similarly, high turbulence in the gas causes the gas layer to be thin.

At the interface, there is a concentration discontinuity and NH<sub>3</sub> occurs at equilibrium across the interface as determined by Henry's law constant. Henry's law constant is a distribution coefficient that expresses the proportionality between the concentration of a gas dissolved in a solvent and its partial pressure (Prausnitz, 1986).

In equation form, Henry's law is

$$P = HC \quad (2)$$

where  $P$  is the partial pressure of the gas,  $C$  is the concentration of the dissolved gas, and  $H$  is the Henry's law constant.

Henry's law constant is a function of temperature for a particular gas-solvent system. Each gas-solvent system, however, has its own unique Henry's law constant. Typically, Henry's law breaks down when partial pressure exceeds 5–10 atmospheres and/or when the dissolved concentration exceeds 3 mol percent (Prausnitz, 1986).

At the interface, there is an equilibrium, and on either side transfer is affected entirely by molecular diffusion. Diffusion occurs when the chemical experiences a drop in potential as a result of the transfer. Volatilization continues until this difference is eliminated and equilibrium is established. According to Mackay (1980), although it is possible to use chemical potential to describe volatilization, it is more convenient to use the concept of chemical fugacity or partial pressure. Therefore, the driving force of diffusion can be regarded as the partial pressure difference between the water and air for the particular gas.

Ammonia in air is in equilibrium with an aqueous solution and generally the concentration of NH<sub>3</sub> in water is many times greater than in the air. There is, therefore, a large concentration gradient across the interface. This, however, is not the controlling factor in the mass transfer. It is generally assumed that there is no resistance at the interface itself, where equilibrium conditions exist. However, the measurements of concentration profiles show that there is a diffusion resistance for gas exchange and it lies in the film on either side of the interface (Coulson *et al.*, 1978; Mackay *et al.*, 1979). Therefore, the controlling factor is the rate of diffusion through the two films where all the resistance exists. This shows that the liquid-phase or gas-phase resistance, or both, determine the overall mass transfer rate of a chemical.

The volatilization of  $\text{NH}_3$ , according to the two-film model, can be described as the diffusion of  $\text{NH}_3$  from the bulk of floodwater to the interface, followed by transfer across the interface, and finally diffusion from the interface to the bulk of the air phase. Ammonia concentrations immediately on either side of the interface are in equilibrium, which is expressed by the Henry's law constant for  $\text{NH}_3$ .

It is interesting to note the views of Danckwerts (1970) in his book on gas-liquid reactions on the two-film model. According to Danckwerts, the two-film model is not entirely realistic and it would not be seriously contended that a discontinuity really exists near the surface, still less that it has a uniform thickness. Nevertheless, the film model incorporates an essential feature of the real system, namely, that the gas must get into the liquid by dissolution and molecular diffusion before it can be transported by convection. He further states that the predictions based on the film model are remarkably similar and sometimes identical to those based on more sophisticated models. In view of its simplicity it is often preferable to use the film model for the purposes of discussion or calculation. Liss (1973) endorsed the concepts of Danckwerts and adapted the two-film model to study gas exchange across an air-water interface. This concept has since been adapted by other researchers and has been used to predict the interfacial transfer of carbon dioxide (Liss, 1973), sulfur dioxide (Liss and Slater, 1974), and various organic chemicals (Liss and Slater, 1974; Mackay and Leiononen, 1975; Dilling, 1977; cohen *et al.*, 1978; Southworth, 1979; Mackay *et al.*, 1979; Rathbun and Tai, 1981; Slater and Spedding, 1981; Smith *et al.*, 1981; Atlas *et al.*, 1982). The two-film model simplifies the theoretical calculation of gas exchange at the air-water interface (Liss and Slater, 1974) and is the most widely used kinetic model in estimating the volatilization of chemicals (Sanders and Seiber, 1984).

### III. THEORY OF AMMONIA VOLATILIZATION

The  $\text{NH}_3$  volatilization process is directly influenced by five primary factors (Jayaweera and Mikkelsen, 1990a). They are floodwater  $\text{NH}_4^+\text{-N}$  concentration, pH, temperature, depth of floodwater, and windspeed. They have developed a theory that describes the effect of these factors on  $\text{NH}_3$  volatilization (Fig. 2) (Jayaweera and Mikkelsen, 1990b).

The rate of  $\text{NH}_3$  volatilization is principally a function of two parameters, (1) the  $\text{NH}_{3(\text{aq})}$  concentration in floodwater, and (2) the volatilization rate constant for  $\text{NH}_3$ ,  $k_{\text{vN}}$ .

$$\text{rate of } \text{NH}_3 \text{ volatilization} = f([\text{NH}_3]_{\text{aq}}, k_{\text{vN}}) \quad (3)$$

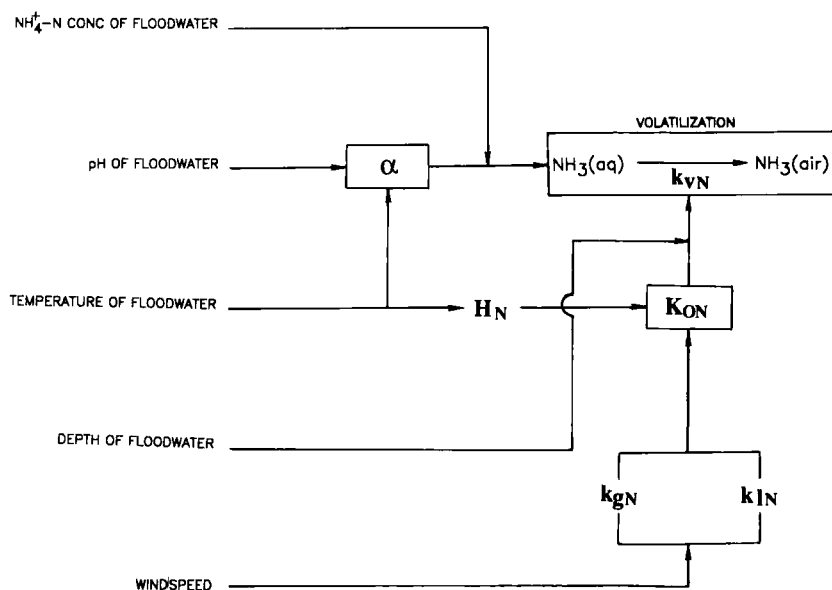


FIG. 2. Theory of NH<sub>3</sub> volatilization in flooded systems:  $\alpha$ , degree of dissociation of NH<sub>4</sub><sup>+</sup>;  $H_N$ ,  $k_{vN}$ ,  $K_{ON}$ ,  $k_{gN}$ , and  $K_{IN}$  are the Henry's law constant, volatilization rate constant, overall mass transfer coefficient, and gas-phase and liquid-phase exchange constants for NH<sub>3</sub>, respectively. (From Jayaweera and Mikkelsen, 1990b.)

Ammonia concentration in floodwater, NH<sub>3(aq)</sub>, is determined by (1) NH<sub>4</sub><sup>+</sup>-N concentration in floodwater, and (2) fraction of dissociation,  $\alpha$  of NH<sub>4</sub><sup>+</sup>. Fraction of dissociation is governed by the dissociation and association rate constants of NH<sub>4</sub><sup>+</sup>/NH<sub>3(aq)</sub> equilibrium, and the H<sup>+</sup> ion concentration in the system as represented by the pH of the medium. Rate constants are ultimately determined by the temperature of the system. Therefore,

$$\text{NH}_{3(\text{aq})} \text{ concentration in floodwater} = f[\text{NH}_4^+\text{-N}], \text{ temperature, pH).} \quad (4)$$

The volatilization rate constant,  $k_{vN}$ , is determined by (1) the depth of floodwater, and (2) the overall mass transfer coefficient for NH<sub>3</sub>, which is influenced by the Henry's law constant for NH<sub>3</sub> and liquid- and gas-phase exchange constants. Henry's law constant is a function of temperature and exchange constants, which are dependent on the windspeed. Therefore,

$$\text{volatilization rate constant for NH}_3 = f(\text{water depth, temperature, windspeed}). \quad (5)$$

By equating Eqs. (4) and (5) to Eq. (3), we obtain

$$\text{rate of NH}_3 \text{ volatilization} = f([\text{NH}_4^+\text{-N}], \text{ temperature, pH, water depth, windspeed}). \quad (6)$$

#### IV. FACTORS AFFECTING AMMONIA VOLATILIZATION

Ammonia volatilization in flooded rice and similar systems is influenced by a variety of water and soil characteristics, fertilizer and crop management practices, and environmental factors (Mikkelsen, 1987). Several floodwater characteristics such as  $\text{NH}_4^+\text{-N}$  concentration, pH,  $\text{P}_{\text{CO}_2}$ , total alkalinity, buffering capacity, temperature, depth, turbulence, and biotic activity influence  $\text{NH}_3$  volatilization. Soil factors affecting  $\text{NH}_3$  volatilization are pH, redox status,  $\text{CaCO}_3$  content, cation exchange capacity, soil texture, and biotic activity. Wind speed, turbulence,  $\text{P}_{\text{NH}_3}$ , air temperature, and solar radiation are several atmospheric conditions influencing  $\text{NH}_3$  volatilization. Nitrogen source, timing, and method of application are three fertilizer management practices affecting  $\text{NH}_3$  loss. Water management can also affect the fluxes controlling the movement of  $\text{NH}_4^+\text{-N}$  between soil, water, and air.

Jayaweera and Mikkelsen (1990a) subdivided these rate-controlling factors into two categories: (1) primary factors, and (2) secondary factors.

##### A. PRIMARY FACTORS AFFECTING $\text{NH}_3$ VOLATILIZATION

Primary factors directly influence the process of  $\text{NH}_3$  volatilization. Numerous secondary factors, however, modify the primary ones.

The primary factors that influence  $\text{NH}_3$  volatilization are  $\text{NH}_4^+\text{-N}$  concentration, pH, temperature, depth of floodwater, and windspeed (Jayaweera and Mikkelsen, 1990a).

##### 1. Effect of Floodwater $\text{NH}_4^+\text{-N}$ Concentration

Volatilization of  $\text{NH}_3$  from floodwater is described as a first-order exponential decay process. Therefore, the rate of  $\text{NH}_3$  volatilization is directly related to the concentration of aqueous  $\text{NH}_3$ , which in turn is a function of  $\text{NH}_4^+\text{-N}$  concentration.

Various researchers have shown a pronounced influence of  $\text{NH}_4^+\text{-N}$  concentration on overall  $\text{NH}_3$  loss (Mikkelsen *et al.*, 1978; Vlek and



Stumpe, 1978; Terman, 1979; Vlek and Craswell, 1979; Bouwmeester and Vlek, 1981a; Denmead *et al.*, 1982; Craswell and Vlek, 1983; Fillery *et al.*, 1984; Fillery and Vlek, 1986; Mikkelsen, 1987; Jayaweera and Mikkelsen, 1990b).

Fillery and Vlek (1986) state that the quantity of NH<sub>4</sub><sup>+</sup>-N in floodwater is an index of the potential NH<sub>3</sub> volatilization and the rate of NH<sub>3</sub> loss is partially dependent on the equilibrium vapor pressure of NH<sub>3</sub> in floodwater. Vlek and Stumpe (1978) reported that the rate of NH<sub>3</sub> volatilization is directly related to the concentration of aqueous NH<sub>3</sub> and therefore to the concentration of NH<sub>4</sub><sup>+</sup>-N and pH. Fertilizer management, through its influence on the concentration of NH<sub>4</sub><sup>+</sup>-N in floodwater, has a pronounced effect on the overall NH<sub>3</sub> loss (Fillery *et al.*, 1984).

Bouwmeester and Vlek (1981a), using their model, showed that the rate of NH<sub>3</sub> volatilization is increased with increasing NH<sub>4</sub><sup>+</sup>-N concentration in floodwater. In a recently developed model by Jayaweera and Mikkelsen (1990b) they showed an increase in NH<sub>3</sub> volatilization with increasing floodwater NH<sub>4</sub><sup>+</sup>-N concentration, under a particular pH, temperature, water depth, and windspeed (Fig. 3). Volatilization rate is increased as a result of an increase in NH<sub>3(aq)</sub> concentration in floodwater. They have further shown that by decreasing pH, temperature, and windspeed, and by increasing the water depth, the NH<sub>3</sub> volatilization rate is decreased at any NH<sub>4</sub><sup>+</sup>-N concentration and vice versa (Fig. 3). A decrease in pH decreases the NH<sub>3(aq)</sub> concentration in floodwater; a decrease in temperature decreases both NH<sub>3(aq)</sub> concentration and the volatilization rate constant, whereas a decrease in windspeed and an increase in floodwater depth decreases only the volatilization rate constant (Jayaweera and Mikkelsen, 1990b). This clearly shows that the NH<sub>3(aq)</sub> concentration at any NH<sub>4</sub><sup>+</sup>-N concentration is an interactive result of various factors associated with the floodwater system.

## 2. Effect of Floodwater pH

Ammonium/ammonia equilibrium is governed by the pH of the medium. Since NH<sub>3</sub> volatilization is directly related to the concentration of aqueous NH<sub>3</sub> in floodwater, pH plays an important role in NH<sub>3</sub> loss. By considering the chemical equilibrium of NH<sub>4</sub><sup>+</sup>/NH<sub>3(aq)</sub> in floodwater, it is possible to relate pH, the equilibrium constant, *K*, and the concentrations as shown in Eq. (7).

$$\text{pH} = \text{pK} + \log \frac{\alpha c}{(1 - \alpha)c} \quad (7)$$

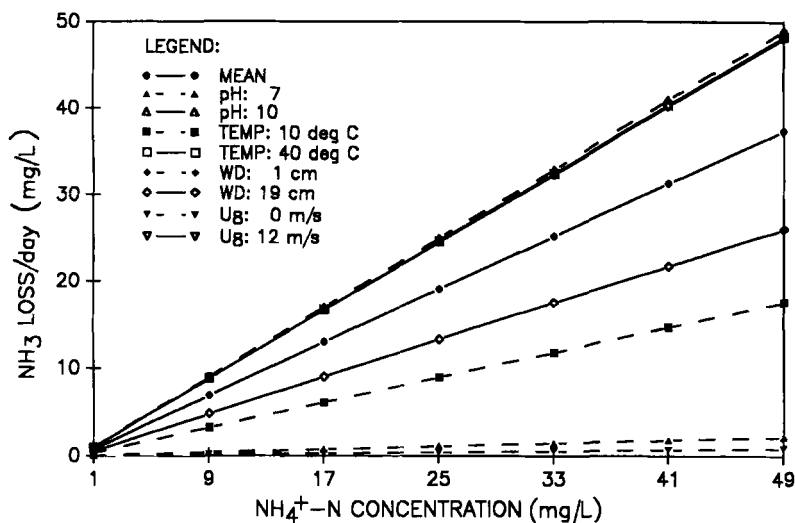


FIG. 3. Effect of floodwater  $\text{NH}_4^+\text{-N}$  concentration on  $\text{NH}_3$  volatilization. MEAN: pH, 8.5; TEMP (temperature),  $25^\circ\text{C}$ ; WD (water depth), 10 cm;  $U_8$  (windspeed at 8 m), 6 m/s. In other simulation runs, all other conditions are maintained constant at their mean values except for the listed variable.

and by rearranging, the fraction of  $\text{NH}_{3(\text{aq})}$   $\alpha$  in the system can be determined:

$$\alpha = \frac{10 \exp(\text{pH} - \text{pK})}{1 + 10 \exp(\text{pH} - \text{pK})} \quad (8)$$

where pH is the pH of floodwater; and pK is  $-\log K$ .

The pK value is temperature dependent. Jayaweera and Mikkelsen (1990a) derived the following expression to compute pK as a function of absolute temperature.

$$\text{pK}(T) = 0.0897 + \frac{2729}{T} \quad (9)$$

where  $\text{pK}(T)$  is  $-\log K$ , equilibrium constant for  $\text{NH}_4^+/\text{NH}_{3(\text{aq})}$  system at absolute Kelvin temperature  $T$ .

By substituting Eq. (9) into (8), they obtained the following expression to compute the fraction of  $\text{NH}_3$  in solution as a function of pH and absolute temperature.

$$\alpha = \frac{10 \exp(\text{pH} - 0.0897 - 2729/T)}{1 + 10 \exp(\text{pH} - 0.0897 - 2729/T)} \quad (10)$$

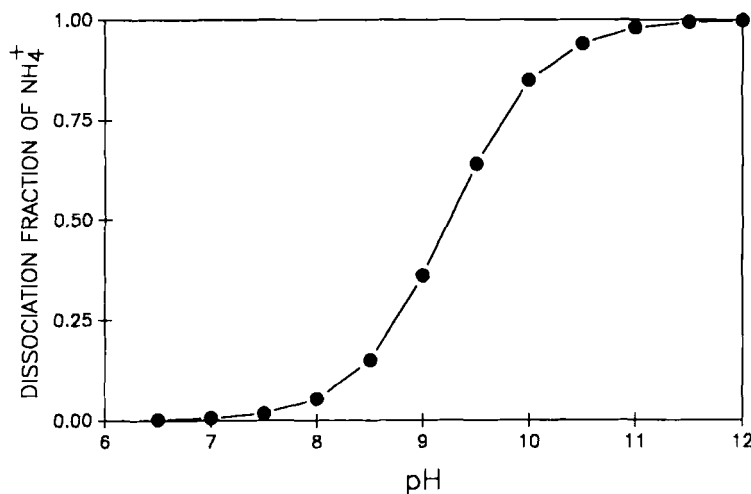


FIG. 4. Effect of pH on fraction of dissociation of NH<sub>4</sub><sup>+</sup>. (From Jayaweera and Mikkelsen, 1990a.)

Figure 4 illustrates the effect of pH on the fraction of dissociation of NH<sub>4</sub><sup>+</sup> (Jayaweera and Mikkelsen, 1990a).

Numerous researchers have shown that floodwater pH has a tremendous impact on NH<sub>3</sub> volatilization (Vlek and Stumpe, 1978; Mikkelsen *et al.*, 1978; Terman, 1979; Bouwmeester and Vlek, 1981a; De Datta, 1981; Vlek and Craswell, 1981; Ferrara and Avci, 1982; Pano and Middlebrooks, 1982; Denmead *et al.*, 1982; Craswell and Vlek, 1983; Fillery *et al.*, 1984; Fenn and Hossner, 1985; Fillery and Vlek, 1986; Jayaweera and Mikkelsen, 1990b). Fenn and Hossner (1985) reported that floodwater pH appears to be the primary contributing factor controlling NH<sub>3</sub> loss from flooded soils. Aqueous NH<sub>3</sub> in floodwater increases about tenfold per unit increase in pH in the range 7.5–9.0 (Vlek and Stumpe, 1978; Vlek and Craswell, 1981), permitting a high level of NH<sub>3</sub> volatilization, but when the pH value is 6.6 or less, there is no removal of NH<sub>3</sub> from a waste water stabilization pond (Pano and Middlebrooks, 1982). Bowmer and Muirhead (1987) reported the importance of pH by demonstrating the change in ratio of NH<sub>3</sub> to NH<sub>4</sub><sup>+</sup> from .056 to 5.6 (at 25°C) as the pH increases from 8.0 to 10.0.

Various models have been used to calculate NH<sub>3</sub> volatilization rates under different conditions such as pH. Bouwmeester and Vlek (1981a) suggested that the effects of pH, wind, and temperature on NH<sub>3</sub> volatilization are of the same order of magnitude. They further stated that for high pH (> ~ 9) the volatilization rate is controlled mainly by the transfer rate

in the liquid diffusion layer, and for low pH the volatilization rate is limited mostly by the  $\text{NH}_3$  transfer rate in the air. Moeller and Vlek (1982) found a correlation between  $\text{NH}_3$  loss and pH that is independent of the volatilization kinetics and this correlation was used experimentally to monitor the  $\text{NH}_3$  volatilization. If sources of extraneous acids and bases are eliminated, the ammoniacal concentrations in solution can be determined by measuring pH. They used this method to gather volatilization data in a series of experiments.

Jayaweera and Mikkelsen (1990b), using their model, showed that an increase in solution pH increases the percentage of  $\text{NH}_3$  loss per day (Fig. 5), as a result of an increase in  $\text{NH}_{3(\text{aq})}$  in floodwater. However, by changing other primary factors such as temperature, depth of floodwater, and windspeed, the  $\text{NH}_3$  volatilization is varied. An increase in temperature from  $10^\circ\text{C}$  to  $40^\circ\text{C}$  increased both the  $\text{NH}_{3(\text{aq})}$  and volatilization rate constant for  $\text{NH}_3$ ,  $k_{\text{vN}}$ , at various pH levels, thus increasing the  $\text{NH}_3$  loss per day. Shallow water enhances  $\text{NH}_3$  loss even at fairly low pH values due to the high volatilization rate constant. On the contrary, with increased water depth,  $\text{NH}_3$  is significantly lost only at high pH values (Fig. 5). This shows

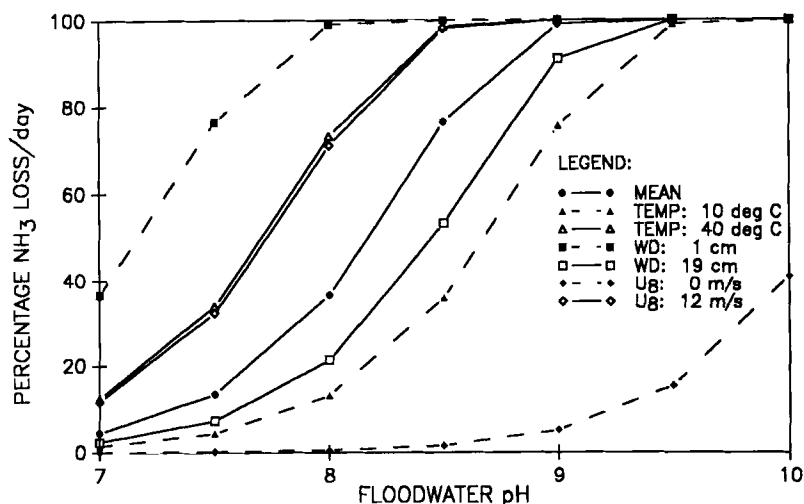


FIG. 5. Effect of floodwater pH on  $\text{NH}_3$  volatilization. MEAN:  $\text{NH}_4^+\text{-N}$  concentration in floodwater, 25 mg/L; pH, 8.5; TEMP (temperature),  $25^\circ\text{C}$ ; WD (water depth), 10 cm;  $U_8$  (windspeed at 8 m), 6 m/s. In other simulation runs, all other conditions are maintained constant at their mean values, except for the listed variable.

that even with high NH<sub>3(aq)</sub> concentrations in floodwater, volatilization can be controlled by low volatilization rate constants, which are achieved by increased water depth. They have further shown that the role of wind-speed is highly significant at various pH levels. At high pH values, NH<sub>3</sub> volatilization is maintained at low values as a result of low windspeed (Fig. 5) due to low volatilization rate constants.

### 3. Effect of Floodwater Temperature

Temperature affects the equilibrium constant of NH<sub>4</sub><sup>+</sup>/NH<sub>3(aq)</sub> system (Bates and Pinching, 1949) and an increase in temperature of floodwater increases the equilibrium constant as shown by Jayaweera and Mikkelsen (1990a). Temperature also influences the Henry's law constant for NH<sub>3</sub>, and using a mathematical model Jayaweera and Mikkelsen (1990a) computed the Henry's law constant for NH<sub>3</sub> as a function of floodwater temperature. The dependency of Henry's law constant on temperature for a particular gas-solvent system is well documented (Burkhard *et al.*, 1985).

In the temperature range typical for tropical climates, NH<sub>3</sub> volatilization is increased by approximately 0.25% per 1°C increase in temperature, suggesting an exponential increase of NH<sub>3</sub> loss with temperature (Vlek and Stumpe, 1978; Terman, 1979). Vlek and Craswell (1981), however, found that at a given NH<sub>4</sub><sup>+</sup>-N concentration, NH<sub>3(aq)</sub> concentration increases in proportion with increasing temperature, which suggests that temperature has an approximately linear effect on NH<sub>3</sub> volatilization.

Temperature influences the rate of NH<sub>3</sub> volatilization in the same order of magnitude as windspeed and pH (Bouwmeester and Vlek, 1981a). An increase in temperature increases the volatilization rate of NH<sub>3</sub> and the NH<sub>3</sub> loss per day (Fig. 6). The higher volatilization rate of NH<sub>3</sub> at high temperature is due to an increased floodwater NH<sub>3(aq)</sub> concentration and the volatilization rate constant for NH<sub>3</sub> (Jayaweera and Mikkelsen, 1990b).

As discussed in the theory for NH<sub>3</sub> volatilization, floodwater NH<sub>3(aq)</sub> concentration and the volatilization rate constant for NH<sub>3</sub> are influenced by the degree of dissociation and the Henry's law constant, respectively (Jayaweera and Mikkelsen, 1990b). They have shown that pH, depth of floodwater, and windspeed influence the NH<sub>3</sub> volatilization process by several orders of magnitude at various temperatures (Fig. 6). Floodwater pH controls the NH<sub>3(aq)</sub> concentration, while the water depth and wind-speed control the volatilization rate constant for NH<sub>3</sub>.

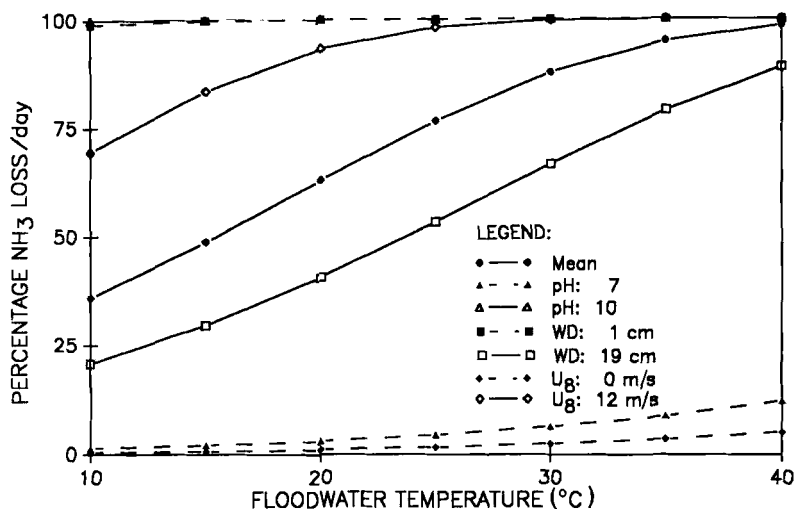


FIG. 6. Effect of floodwater temperature on  $\text{NH}_3$  volatilization. MEAN:  $\text{NH}_4^+\text{-N}$  concentration in floodwater, 25 mg/L; pH, 8.5; TEMP (temperature), 25°C; WD (water depth), 10 cm;  $U_8$  (windspeed at 8 m), 6 m/s. In other simulation runs, all other conditions are maintained constant at their mean values, except for the listed variable.

#### 4. Effect of Water Depth

The role of depth of floodwater in  $\text{NH}_3$  volatilization is twofold. Primarily it affects  $\text{NH}_4^+$ -ion concentration by virtue of its dilution effect. Further, it influences the volatilization relationships  $k_{vN}$  (Jayaweera and Mikkelsen, 1990a) that have not been addressed in previous research.

All transformations in an ecosystem, such as  $\text{NH}_3$  transfer across the water–air interface, must obey the law of conservation of mass. To avoid any violation, therefore, it is important to consider the material balance of the system (Neely, 1980).

For interpretation, suppose there is a container of water, depth  $d$ , containing  $\text{NH}_{3(aq)}$  which is volatilized from the surface via a first-order reaction process. By dimensional analysis, the material balance of this system can be determined as

$$\frac{dC_N}{dt} V = K_{ON} C_N A \quad (11)$$

where  $C_N$  is the  $\text{NH}_{3(aq)}$  concentration in the solution, mol/ $L^3$ ;  $V$  is the volume of the solution,  $L^3$ ;  $A$  is the area of the surface,  $L^2$ ;  $K_{ON}$  is the overall mass transfer coefficient for  $\text{NH}_3$ ,  $L/t$ ;  $L$  is the length; and  $t$  is the time.

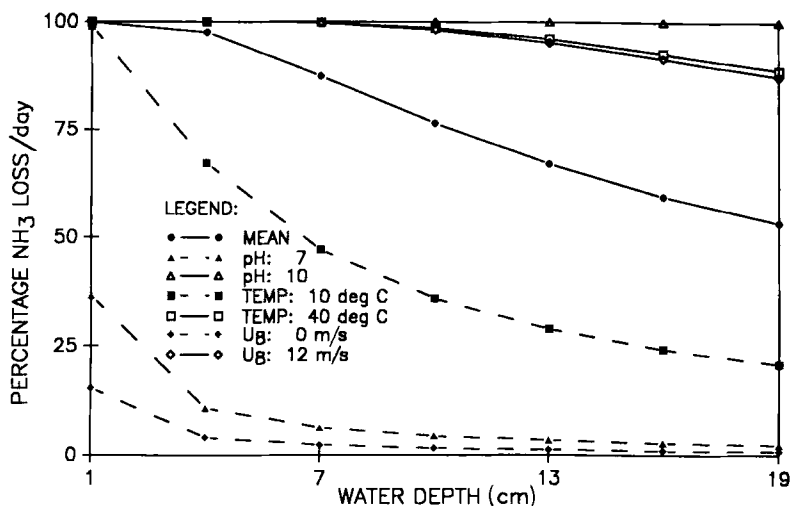


FIG. 7. Effect of floodwater depth on NH<sub>3</sub> volatilization. MEAN: NH<sub>4</sub><sup>+</sup>-N concentration in floodwater, 25 mg/L; pH, 8.5; TEMP (temperature), 25°C; WD (water depth), 10 cm; U<sub>8</sub> (windspeed at 8 m), 6 m/s. In other simulation runs, all other conditions are maintained constant at their mean values, except for the listed variable.

Dividing Eq. (11) by  $V$  yields

$$\frac{dC_N}{dt} = \frac{K_{ON}}{d} C_N \quad (12)$$

where  $d$  is the depth of solution in the container.

The ratio  $K_{ON}/d$  is a first-order volatilization rate constant for NH<sub>3</sub>,  $k_{vN}$

$$k_{vN} = \frac{K_{ON}}{d} \quad (13)$$

In the case of flooded systems,  $d$  represents the mean depth of floodwater. This relationship shows that the volatilization rate constant for NH<sub>3</sub> is inversely related to the depth of floodwater. The volatilization rate constant,  $k_{vN}$ , and the half-life,  $t_{1/2}$  ( $0.693/k_{vN}$ ) for NH<sub>3</sub> desorption are calculated as a function of floodwater depth by using the model developed by Jayaweera and Mikkelsen (1990a). An increase in depth of floodwater decreases the volatilization rate constant,  $k_{vN}$ , and increases the half life,  $t_{1/2}$ .

Using computer simulation runs, Jayaweera and Mikkelsen (1990b) showed that as the depth of floodwater increases from 1 to 19 cm, the volatilization rate of NH<sub>3</sub> loss per day decreases from 100 to 53% (Fig. 7). This is due to a decrease in volatilization rate constant,  $k_{vN}$  when other factors are maintained at constant values (NH<sub>4</sub><sup>+</sup>-N concentration,

25 mg/L; pH, 8.5; temperature, 25°C; and windspeed at 8 m height, 6 m/s). As shown in Fig. 7, at any particular water depth and at a constant  $\text{NH}_4^+\text{-N}$  concentration, an increase in pH, temperature, and windspeed increases the percentage of  $\text{NH}_3$  loss and vice versa. It is interesting to note that, by managing the depth of floodwater, it is possible to modify  $\text{NH}_3$  losses from flooded systems.

Thibodeaux (1979) showed the fraction of  $\text{NH}_3$  desorbed with water depth for a small stream in southern Arkansas. For example, at pH 8.0 and temperature 60°F, nearly 90% of  $\text{NH}_3$  is desorbed at 0.1 ft water depth, about 70% is lost at 0.5 ft, and around 20% of  $\text{NH}_3$  is lost at a depth of 1 ft during the same duration of time. According to Thibodeaux, the volatilization of  $\text{NH}_3$  from deep rivers is significantly lower than in small streams mainly because of water depth.

### 5. Effect of Windspeed

Kanwisher (1963) showed that at low windspeeds, there is little effect on the gas exchange rates until a critical value is reached. At this unique speed, the wind gets a better "grip" on the water surface. Cohen *et al.* (1978) also reported the importance of wind effect above a critical speed, and accordingly, above the critical speed, shear stress at the interface is large enough to set the interface and the liquid below in motion. Above the critical value, the exchange rate is supposed to increase as the square of the windspeed (Kanwisher, 1963). Broecker and Peng (1974) reported the same observations. Therefore, gusty winds may account for a large fraction of the exchange, even though they are only of short duration.

Water waves, created as a result of high windspeeds, tend to increase the interfacial area directly. However, Kinsman (1965) reported that wave height to wave length ratio is probably at most 0.143, and according to Cohen *et al.* (1978) this wave height to wave length ratio cannot account for more than a 4% increase in transfer rate.

Several researchers have shown that windspeed is an important environmental parameter in  $\text{NH}_3$  volatilization. Fillery *et al.* (1986a) concluded that high windspeeds in the field promoted  $\text{NH}_3$  loss and probably precluded any important N loss via nitrification-denitrification. Vlek and Stumpe (1978) reported that the relation between the loss of  $\text{NH}_3$  from solution and the air exchange rate is curvilinear with a rapid increase in  $\text{NH}_3$  volatilization at the lower flow rates that they tested. Several researchers observed a linear relationship between  $\text{NH}_3$  loss and windspeed in field experiments (Fillery *et al.*, 1984; Fillery and Vlek, 1986). Denmead *et al.* (1982) showed that  $\text{NH}_3$  volatilization increased with the approxi-



mate square of windspeed in furrow irrigated maize, implying an exponential increase in NH<sub>3</sub> volatilization with windspeed. In a recent greenhouse study, Katyal and Carter (1989) reported that the relationship between airflow rate and NH<sub>3</sub> loss was logarithmic rather than linear in nature, and they concluded that this may be due to cooling of floodwater associated with high air flow rates.

These various relationships observed by researchers may be due to the variety of conditions that they encounter in their experiments. Jayaweera and Mikkelsen (1990b), by using model simulation runs, showed the effect of windspeed on NH<sub>3</sub> volatilization under various conditions (Fig. 8). They show clearly that the nature of the relationship changes tremendously depending on existing conditions. For example: at pH 10.0, all the NH<sub>4</sub><sup>+</sup>-N in floodwater is lost at a windspeed as low as 2 m/s at 8 m height, compared to 12% loss at 12 m/s windspeed when the pH is 7.0. This illustrates that even with a high volatilization rate constant, if the NH<sub>3(aq)</sub> in floodwater is low, only a small amount of NH<sub>3</sub> is lost. Bouwmeester and Vlek (1981a), using their diffusion model found that at low windspeeds the volatilization rates are very small, and the gas-phase resistance dominates. However, with increasing windspeed the volatilization rates increase, and the liquid-phase resistance becomes more significant due to depletion of NH<sub>3</sub> in the

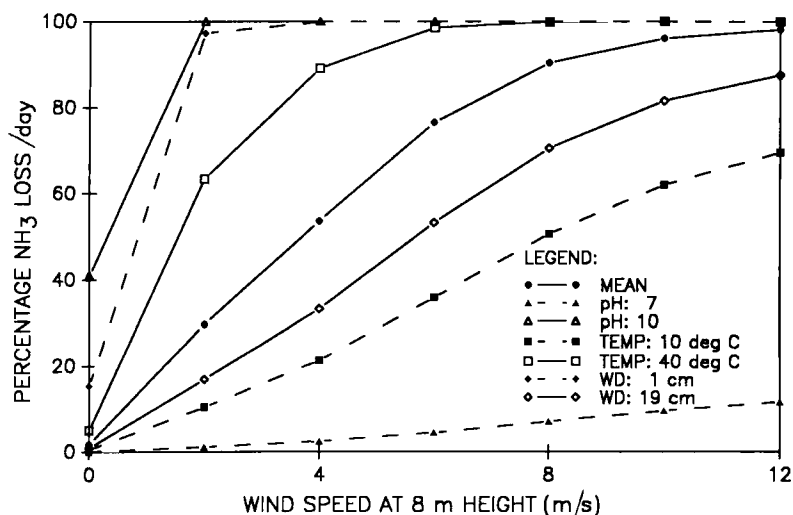


FIG. 8. Effect of windspeed on NH<sub>3</sub> volatilization. MEAN: NH<sub>4</sub><sup>+</sup>-N concentration in floodwater, 25 mg/L; pH, 8.5; TEMP (temperature), 25°C; WD (water depth), 10 cm; U<sub>8</sub> (windspeed at 8 m), 6 m/s. In other simulation runs, all other conditions are maintained constant at their mean values, except for the listed variable.

surface film of the liquid phase. They reported that this shift from gas-phase resistance to liquid-phase resistance is more evident at high pH values.

Fillery and Vlek (1986) reported that there was a good fit ( $R^2 = 0.90$ ) in the following relationship between the partial pressure of  $\text{NH}_3$  ( $P_{\text{NH}_3}$ ) in the floodwater and windspeed at 1.2 m ( $W_2$ ) during the volatilization process.

$$F = k P_{\text{NH}_3} W_2 \quad (14)$$

where  $F$  is the flux of  $\text{NH}_3$ , and  $k$  is a constant.

Windspeed, however, influences the  $\text{NH}_3$  volatilization process by virtue of its role on the volatilization rate constant (Jayaweera and Mikkelsen, 1990a,b). Other factors such as temperature, pH, and depth of floodwater, however, could vary the rate of volatilization depending on the conditions.

## B. SECONDARY FACTORS AFFECTING AMMONIA VOLATILIZATION

Secondary factors influence the primary factors in the process of  $\text{NH}_3$  volatilization. Each primary factor is a function of several secondary factors. Thus, the  $\text{NH}_3$  volatilization process is the overall result of numerous characteristics of soil, water, fertilizer management, and atmospheric conditions.

### 1. Effect of Secondary Factors on Floodwater $\text{NH}_4^+\text{-N}$ Concentration

Ammonia volatilization is generally influenced most by the factors that influence the  $\text{NH}_4^+\text{-N}$  concentration in floodwater. Mikkelsen *et al.* (1978) showed that higher concentrations of  $\text{NH}_4^+\text{-N}$  in rice floodwater increased  $\text{NH}_3$  volatilization losses. Nitrogen source, rate and method of application, soil CEC, biotic component such as urease activity, assimilation by algae, weeds, and rice, and immobilization by soil components are important secondary factors that influence  $\text{NH}_3$  volatilization.

The source of fertilizer N plays an important role in determining the  $\text{NH}_4^+\text{-N}$  concentration in floodwater, thereby influencing the  $\text{NH}_3$  volatilization. Urea is currently the most important fertilizer source in rice cultivation, followed by ammonium sulfate. Freney *et al.* (1985) reported that there is a worldwide move to use urea as the primary form of fertilizer N.

Urea is hydrolyzed by the urease enzyme to form  $(\text{NH}_4)_2\text{CO}_3$  (Fenn and Hossner, 1985) and  $\text{NH}_4^+$ , whereas  $(\text{NH}_4)_2\text{SO}_4$  provides  $\text{NH}_4^+$  directly into

the system. The kinetics of urea hydrolysis in moist soils have given different results. Some researchers reported that urea hydrolysis is a first-order reaction with respect to urea concentration (Overrein and Moe, 1967; Sankhayan and Shukla, 1976). Recent studies, however, showed zero-order kinetics for urea hydrolysis (Sahrawat, 1980; Vlek and Carter, 1983). In flooded soils, Eriksen and Kjeldby (1987) reported that urea hydrolysis exhibited a zero-order reaction when urea super granules were point-placed at a 10-cm soil depth.

There are numerous reports comparing the effect of urea and (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> in NH<sub>3</sub> volatilization. When (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> is applied to puddled soil, Vlek and Stumpe (1978) observed nearly 11% of the N applied was lost as NH<sub>3</sub>. Vlek and Craswell (1979), however, found a higher rate of loss (50% N applied) when urea is applied. These findings show that urea is more prone to N losses in flooded soils.

Recently, Fillery and De Datta (1986) reported NH<sub>3</sub> fluxes of up to 38 and 36% of the N applied from (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> and urea, respectively. In several other field studies, high losses of N have been detected following the application of urea and (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> (Craswell *et al.*, 1985; Katyal *et al.*, 1985; Vlek and Byrnes, 1986). These findings confirm the earlier reports of Mikkelsen *et al.* (1978) and Vlek and Craswell (1979), but contradict other studies (MacRae and Ancajas, 1970; Ventura and Yoshida, 1977; Wetselaar *et al.*, 1977; Freney *et al.*, 1981). These contradictions may be due to the differences in the alkalinity of various sources of water used to irrigate flooded rice (Vlek and Stumpe, 1978; Vlek and Craswell, 1979). Fillery *et al.* (1986b), however, in trying to explain these contradictions reported that alkalinity in floodwater as a result of evaporation and/or respiration contributed to the rapid loss of NH<sub>3</sub> following the application of (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> and urea to the floodwater.

Even though there may be the same amount of NH<sub>3</sub> loss from urea and (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>, the pattern of loss differed between these fertilizers in an 8-day period. Several researchers detected NH<sub>3</sub> fluxes immediately after the application of (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> to flooded soils (Freney *et al.*, 1981; Fillery and De Datta, 1986; Fillery *et al.*, 1986b) and within 2–4 hours after the application of urea (Freney *et al.*, 1981; Simpson *et al.*, 1984; Fillery and De Datta, 1986; Fillery *et al.*, 1986b). Maximum NH<sub>3</sub> fluxes are generally observed immediately following the application of (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> (Mikkelsen *et al.*, 1978; Freney *et al.*, 1981; Fillery and De Datta, 1986; Fillery *et al.*, 1986b) or a few days after the urea application (Freney *et al.*, 1981; Fillery *et al.*, 1984, 1986b; Fillery and De Datta, 1986). The different pattern of NH<sub>3</sub> fluxes from urea and (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> were primarily due to the differences in the pattern of NH<sub>4</sub><sup>+</sup>-N concentration in floodwater (Wetselaar *et al.*, 1977; Fillery *et al.*, 1986b).

There has been an interest in modifying the dissolution rate of urea by

coating the granules, adding chemical additives, by increasing the particle size of the granule, or formulation of controlled release materials.

Sulfur-coated urea (SCU), in particular, is known to be an effective N source for rice (De Datta and Gomez, 1981; De Datta *et al.*, 1983; Flinn *et al.*, 1984; Katyal *et al.*, 1985; Buresh, 1987; Rao, 1987). Craswell *et al.* (1981) reported that  $\text{NH}_4^+\text{-N}$  concentrations in floodwater are much lower after basal incorporation of SCU than after urea applications.

Lac-coated urea (LCU), urea coated with shellac resin, however, was ineffective in reducing peak ammoniacal N levels or losses (Rao, 1987). Phosphate rock-coated urea (PRCU), an experimental material prepared by Madras Fertilizer Limited, Madras, India (Buresh, 1987), has been field evaluated with rice in India, and comparable rice yields for PRCU and urea have been reported (Singh and Yadav, 1985).

Guanyl urea sulfate (GUS) is a slowly mineralized source of N by microbial action under aerobic and anaerobic conditions (Davies, 1976; Ebisuno and Takimoto, 1981; Buresh, 1987). Ammonia formation and presumably loss were least for GUS according to Buresh (1987) who reported that the negligible  $\text{NH}_3$  concentration in floodwater may be due to the slow mineralization and acidifying effect of GUS.

Urea phosphate, which is known to produce an acidifying effect and to reduce loss of urea N as  $\text{NH}_3$  (Bremner and Douglas, 1971a; Stumpe *et al.*, 1984), failed to reduce  $\text{pNH}_3$  under flooded condition due to the stimulation of algal photosynthetic activity by added P (Buresh, 1987).

Urea-forms, which are condensation products of urea and formaldehyde, were less prone to  $\text{NH}_3$  loss than urea in a greenhouse study with rice (Carter *et al.*, 1986) and in a field study (Buresh, 1987). This may be due to the slow release of N from urea forms through microbial action (Corke and Robinson, 1966).

Rao (1987) reported that urea supergranules (USG), spherical granules of 1 g each, reduced the peak  $\text{NH}_4^+\text{-N}$  levels to  $<2 \text{ g/m}^3$  and N losses to 3.9%. Eriksen and Kjeldby (1987) reported that  $\text{NH}_3$  volatilization was noticeably reduced by the surface application of urea calcium nitrate (UCN) on flooded soil as compared with USG. According to them, the total N loss from USG after 30 days was 17% of applied urea, but when the same amounts of urea and nitrogen were applied as UCN this loss was reduced to 3% and 6%, respectively.

Rate of N application obviously should control the amount of  $\text{NH}_4^+\text{-N}$  that comes into the floodwater. Vlek and Craswell (1979) reported that reduced N application rates reduced  $\text{NH}_3$  volatilization by lowering the level of  $\text{NH}_4^+\text{-N}$  in floodwater. MacRae and Ancajas (1970), in a laboratory study, found that an increased application of both  $(\text{NH}_4)_2\text{SO}_4$  and urea resulted in increased losses of  $\text{NH}_3$  through volatilization. Fenn and Hossner (1985) reported the same.

Method of N fertilizer application influences the ammoniacal N concentration in floodwater (Fillery *et al.*, 1984) and therefore plays an important role in NH<sub>3</sub> volatilization. Basically, there can be three ways of applying fertilizer N to flooded soils: (1) broadcast application; (2) broadcast and incorporation; and (3) deep placement. Broadcast applications can be done in several different ways. They are: broadcast as a basal dose, broadcast as a top-dressing at different stages of crop growth, or broadcast and incorporate the fertilizer material into the soil. Deep placement is a practice that places the fertilizer in the reduced layer of the flooded soil so that the concentration of urea and NH<sub>4</sub><sup>+</sup> in floodwater remains essentially zero. This can be done in several ways, namely soil injection, mud ball placement, drill placement, band placement, or point placement.

In the last decade, there have been numerous papers published on aspects of N fertilizer management. Mikkelsen *et al.* (1978) reported considerable losses of NH<sub>3</sub> when urea and (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> were applied directly to floodwater, but less than 1% of the total N applied was volatilized when N fertilizer was placed at a depth of 10–12 cm. In a paper presented at the 14th International Congress of Soil Science, Kyoto, Japan (August 12–18, 1990), Rolston and his co-workers in a simulation study showed that the amount of NH<sub>3</sub> volatilization is affected by windspeed for the cases of NH<sub>4</sub><sup>+</sup>-N fertilizer applied to the floodwater and incorporated into the soil (Fig. 9) (Rolston *et al.*, 1990). Deep placement reduces the NH<sub>3</sub> volatilization largely by reducing the NH<sub>4</sub><sup>+</sup>-N level in floodwater. Vlek and Craswell (1979), MacRae and Ancajas (1970), Fillery *et al.* (1984), and Ericksen *et al.* (1985) reported the same.

Uniform placement of prilled urea and point placement of urea super granules have given low total N (urea + NH<sub>4</sub><sup>+</sup>-N) concentration in floodwater and demonstrates that these methods can be used to reduce N losses in lowland rice production (Cao *et al.*, 1984).

The highest concentrations of NH<sub>4</sub><sup>+</sup>-N and highest level of NH<sub>3</sub> have been detected when urea or (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> was applied to floodwater 2–4 weeks after the transplanting Fillery *et al.*, 1984, 1986b). Rao (1987) found the highest concentrations of NH<sub>4</sub><sup>+</sup>-N in floodwater and NH<sub>3</sub> loss when granular urea was applied wholly as a basal dose.

Higher total N concentration in floodwater was recorded after split application (2/3 basal-broadcast and incorporated, and 1/3 top-dressed, 5–7 days before panicle initiation) than in band placement of urea, indicating greater potential for NH<sub>3</sub> volatilization (Cao *et al.*, 1984). Rao (1987), however, reported that a split urea application (1/2 at transplanting, 1/4 each at 21 days and 42 days after transplanting of rice) reduced peak NH<sub>4</sub><sup>+</sup>-N levels and NH<sub>3</sub> volatilization losses. The differences in their conclusions may be due to timing and amount of split application. The observations of Cao *et al.* (1984), however, show that substantial N

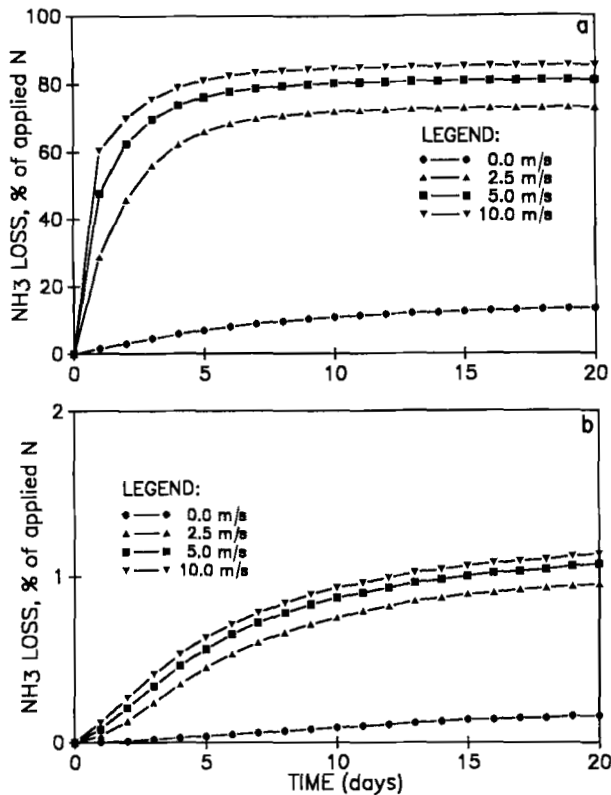


FIG. 9. Ammonia volatilization as affected by windspeed under two different fertilizer managements: (a)  $\text{NH}_4^+$ -N fertilizer applied to floodwater; and (b)  $\text{NH}_4^+$ -N fertilizer incorporated into soil. Water depth and pH are constant at 5 cm and 8.5, respectively. (Adapted from Rolston *et al.*, 1990.)

losses can still occur when N is broadcast and incorporated before transplanting.

Draining the floodwater from the soil and incorporating urea before transplanting reduced the extent of N loss (Fillery *et al.*, 1986a). Cao *et al.* (1984) also reported reduced losses and high  $^{15}\text{N}$  recovery following a thorough incorporation of urea. However, high concentrations of  $\text{NH}_4^+$ -N are found in floodwater (Craswell *et al.*, 1981; Cao *et al.*, 1984) and substantially lower  $^{15}\text{N}$  recoveries have been reported when incorporation is attempted without first removing the floodwater (Cao *et al.*, 1984; Craswell *et al.*, 1985). Therefore, it appears necessary to drain the floodwater from puddled soils before the application of urea if high N crop efficiency is to be achieved without deep placement of fertilizer (Fillery *et al.*, 1986a). It

is interesting to note that Buresh (1987) reported that thorough incorporation of GUS and SCU is not necessary to prevent NH<sub>3</sub> loss.

With all this information, it is easy to conclude that with fertilizers such as urea and (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>, deep placement reduces NH<sub>3</sub> volatilization, and applying ammoniacal N fertilizer into floodwater can lead to large losses of gaseous N. Nonetheless, Asian farmers still frequently broadcast N fertilizer without subsequent incorporation into the soil (Mikkelsen *et al.*, 1978; De Datta, 1981). This practice may occur because small-scale farmers prefer to apply their fertilizer only after the crop is established and broadcast application is the only mode of application at that time (Freney *et al.*, 1985).

Cation exchange capacity (CEC) of a soil affects the retention capacity of a soil for cations. CEC could potentially affect NH<sub>4</sub><sup>+</sup> concentration in floodwater, which indirectly influences the extent of NH<sub>3</sub> loss (Vlek and Craswell, 1979; Freney *et al.*, 1983). Several researchers have found an inverse relationship of NH<sub>3</sub> volatilization to CEC of the soil (Overrein and Moe, 1967; Matocha, 1976; Fenn and Kissel, 1976; Fenn *et al.*, 1982; Fenn and Hossner, 1985; Mikkelsen, 1987). Recently, however, Eriksen and Kjeldby (1987) found low NH<sub>3</sub> loss from urea super granules in a soil with low CEC. Fleisher *et al.* (1987) in a model of NH<sub>3</sub> volatilization from calcareous soils reported that most NH<sub>3</sub> loss is due to the interactive effect of high soil pH and low CEC.

Because of the dynamic nature of soil CEC, it is easy to understand why there is no consistent agreement among researchers regarding the relationship of CEC to NH<sub>4</sub><sup>+</sup> retention.

Biotic activity in a flooded rice ecosystem could have a dominant role in controlling the NH<sub>4</sub><sup>+</sup> concentration in floodwater. Urease activity (Freney *et al.*, 1983; Mikkelsen, 1987), assimilation of NH<sub>4</sub><sup>+</sup>-N by algae, weeds, and rice plant (Craswell *et al.*, 1985), and immobilization of N in the soil (Freney *et al.*, 1983) could control the NH<sub>3</sub> volatilization by influencing the NH<sub>4</sub><sup>+</sup> concentration.

As mentioned earlier, urease activity could follow zero-order or first-order kinetics (Overrein and Moe, 1967; Sankhayan and Shukla, 1976; Sahrawat, 1980; Vlek and Carter, 1983; Eriksen and Kjeldby, 1987). Depending on the degree of urease activity, urea can provide NH<sub>4</sub><sup>+</sup> to the flooded system. According to Fenn and Hossner (1985), NH<sub>3</sub> loss from flooded soils is favored by urease activity.

There have been many attempts to control the reaction rate of urease with metabolic inhibitors (Bremner and Douglas, 1971b) using toxic heavy metals and organic compounds. Vlek *et al.* (1980) showed that phenyl phosphodiamide (PPD), added at a rate of 2% (w/w) delays the appearance of NH<sub>3</sub> in floodwater after broadcasting urea. Application of PPD (1%

w/w) with urea inhibited urease activity for up to 3 days in a field study (Fillery and De Datta, 1986; Fillery *et al.*, 1986c). Fillery *et al.* (1986c) suggested that the effect of PPD on  $\text{NH}_3$  volatilization is largely a function of the delay in the buildup of  $\text{NH}_4^+\text{-N}$  in the floodwater and not as a result of delaying the increase in pH of floodwater as suggested by Byrnes *et al.* (1983). Byrnes *et al.* (1983) showed that PPD (1% w/w) inhibited urease activity for up to 11 days. These differences may be due to the variations in the rate of degradation of PPD under various conditions. Austin *et al.* (1984) showed that PPD degradation is highly dependent on pH and temperature.

From these observations it is clear that PPD seems to decompose rapidly in flooded soils. Therefore, more effective urease inhibitors are needed to minimize the accumulation of  $\text{NH}_4^+\text{-N}$  in floodwater to reduce  $\text{NH}_3$  volatilization after urea application (Fillery and Vlek, 1986).

Nonetheless, controlling  $\text{NH}_3$  loss by inhibiting urease enzyme is a worthy effort, but the ultimate urease inhibitor, however, should be specific to urease, inexpensive, effective in low concentrations, and should not pollute the environment.

Craswell *et al.* (1985) have shown that a significant quantity of  $^{15}\text{N}$  (15% N applied) can be detected in algae and weeds after 2 weeks of urea application. This may reduce  $\text{NH}_3$  loss by virtue of low  $\text{NH}_4^+\text{-N}$  concentration in floodwater. Craswell *et al.* (1981) found low  $\text{NH}_3$  loss when N fertilizer is applied when root systems are well developed.

## 2. Effect of Secondary Factors on Floodwater pH

Floodwater pH is the resultant interaction of several properties including concentration of dissolved  $\text{CO}_2$  and  $\text{NH}_3$ , biotic activity, alkalinity, pH buffering capacity, and temperature (Keeney and Sahrawat, 1986). These floodwater properties are influenced by other practices such as fertilizer management, water quality, and the stage of crop development (Mikkelsen *et al.*, 1978).

Ponnamperuma (1978) reported that the pH of floodwater is largely a function of  $\text{CO}_2$  concentration and  $\text{HCO}_3^-$  activity.

$$\text{pH} = 7.85 + \log (\text{HCO}_3^-) - P_{\text{CO}_2} \quad (15)$$

Constant removal of  $\text{CO}_2$  may increase the pH and addition of  $\text{CO}_2$  may decrease the pH of floodwater. Mikkelsen *et al.* (1978) found a relationship between floodwater pH and the biotic activity. They observed a diurnal change in pH, which appears to be synchronized with the cycle of photosynthesis and respiration. They reported pH values as high as 9.5–10.0 by



midday and decreasing as much as 2–3 pH units during the night (Fig. 10). Several others reported the biotic influence on floodwater pH (Park *et al.*, 1958; Mikkelsen and De Datta, 1979; Craswell *et al.*, 1981; Morel, 1983; Fillery *et al.*, 1984). It is interesting to note that Bowmer and Muirhead (1987) were able to dampen the diurnal fluctuation in pH for 6 days, and significantly increased the ammoniacal N concentration in floodwater by using a photosynthetic inhibitor, terbutryne [2-(*tert*-butylamino)-4-(ethylamino)-6-(methylthio)-S-triazine].

Bouldin (1986) summarized the sequence of events that happens during the day. Photosynthesis depletes CO<sub>2</sub>, increases pH, and increases partial

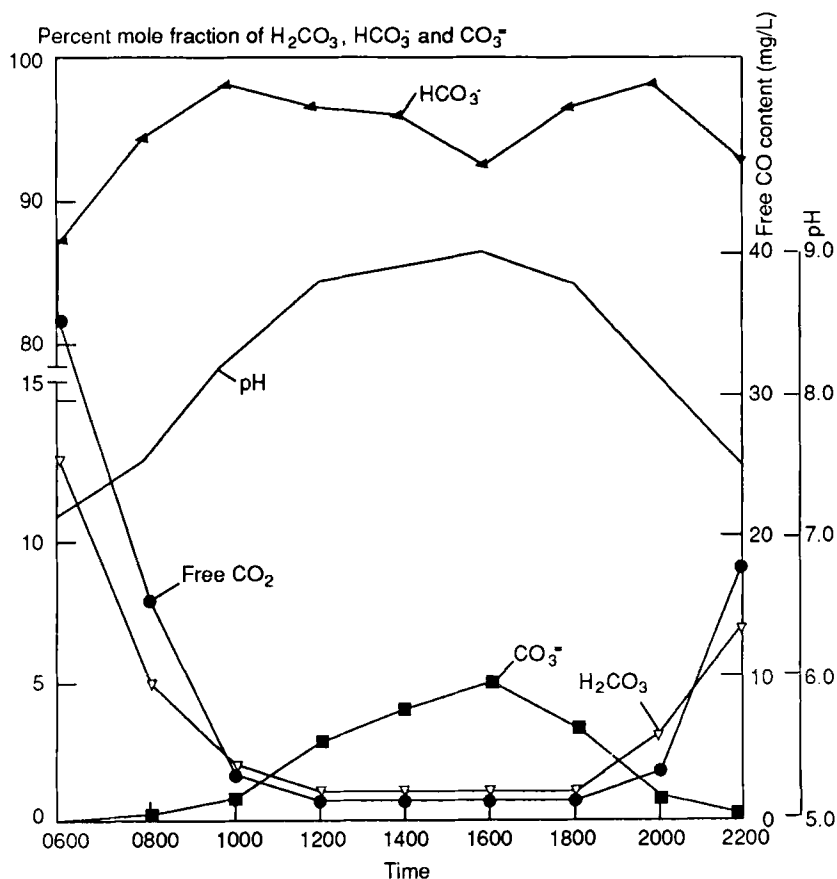


FIG. 10. Changes in the pH and components of the carbonic acid system of rice floodwater 3 days after application of N fertilizer on Maahas clay, Los Baños, Philippines, 1976 wet season. (From Mikkelsen *et al.*, 1978.)

pressure of  $\text{NH}_3$ . Therefore,  $\text{NH}_3$  volatilization is increased during the day. At night, as respiration supplies  $\text{CO}_2$ , the sequence of events are reversed and the  $\text{NH}_3$  volatilization is decreased.

Fillery *et al.* (1986b) reported that the algal enumerations in their study showed relatively low algal biomass. Nevertheless, they observed large fluctuations in pH of floodwater. This study shows that large algal populations are not required to increase floodwater pH to high values that support rapid  $\text{NH}_3$  loss. Growth of algal biomass, however, is not a limitation in most rice growing ecosystems. Pantastico and Suaya (1974) reported that algal biomass is often regarded as a problem in rice floodwater in the Philippines. In Australia, large populations of diatoms and other algae sometimes smother the young rice seedlings (Dunigan and Hill, 1977), while in Bengal at least 1 million ha of transplanted rice are infested with stonewarts (Mukherji, 1968).

The alkalinity of water is a measure of its capacity to accept protons. In natural waters, the alkalinity is generally established by the concentration of  $\text{HCO}_3^-$ ,  $\text{CO}_3^{2-}$ , and  $\text{OH}^-$  ions. Other species, such as  $\text{NH}_3$ , silicates, borates, and phosphates in natural waters may also contribute to the alkalinity of the system. Alkalinity and acidity are interrelated. Basically, acidity and alkalinity are a good measure of the buffering capacity of a given system.

Ammonia volatilization is an acidifying process due to the release of  $\text{H}^+$  to the system. If there is no alkalinity in the floodwater, the pH may decrease and thereby reduces  $\text{NH}_3$  volatilization. According to Vlek and Stumpe (1978), to sustain  $\text{NH}_3$  volatilization, alkalinity (chiefly  $\text{HCO}_3^-$ ) must be present in floodwater to buffer the production of  $\text{H}^+$ .

Several sources may provide alkalinity to floodwater. In Asia, artesian or ponded water is chiefly used as the irrigation source for dry-season rice crops (Stangel, 1979) and it may provide sufficient alkalinity to buffer the system. Vlek and Craswell (1981) reported that sufficient alkalinity can be found in areas with calcareous soils or when soils are irrigated with alkaline well waters. When N forms such as  $(\text{NH}_4)_2\text{SO}_4$  or  $(\text{NH}_4)_2\text{HPO}_4$  are used, irrigation water is probably the major source of alkalinity in floodwater systems (Fillery and Vlek, 1986). However, Fillery *et al.* (1986b) reported that regardless of the quality of irrigation water applied at the time of fertilizer application, the alkalinity in the floodwater can increase through evaporation or other processes. This highlights the likelihood that many flooded rice fields in Asia could contain an adequate quantity of alkalinity with modest rates of  $\text{NH}_3$  loss from  $\text{NH}_4^+\text{-N}$ .

Urea hydrolysis produces  $\text{HCO}_3^-$  that can buffer  $\text{H}^+$  production when urea is used as the fertilizer. Therefore,  $\text{NH}_3$  loss from urea is less dependent on inherent alkalinity (Vlek and Craswell, 1981). Ammonium sulfate

application, on the other hand, will lead to NH<sub>3</sub> volatilization only if the aqueous system is alkaline (Vlek and Stumpe, 1978).

As discussed before, the various differences that had been reported (MacRae and Ancajas, 1970; Wetselaar *et al.*, 1977; Ventura and Yoshida, 1977; Mikkelsen *et al.*, 1978; Vlek and Craswell, 1979; Freney *et al.*, 1981; Craswell *et al.*, 1985; Katyal *et al.*, 1985; Fillery and De Datta, 1986; Fillery *et al.*, 1986b; Vlek and Byrnes, 1986) in NH<sub>3</sub> fluxes for (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> and urea may be due to the degree of buffering capacity in floodwater as a result of alkalinity in the system.

Fertilizer management and the stage of crop development influence the magnitude of diurnal fluctuations in pH of floodwater, presumably because of their effect on the algal biomass (Mikkelsen *et al.*, 1978).

Terman (1979) reported that both N and P fertilizer contribute to algal bloom accompanied by higher water pH. Urea phosphate fertilizers promoted rapid algal growth immediately following either basal incorporation or broadcast application into floodwater (Buresh, 1987). He suggested that this elevation in pH was apparently due to the stimulation of algal photosynthetic activity by added P, and it may explain the failure of a phosphoric acid amendment to urea (urea phosphate) in reducing pNH<sub>3</sub>.

Fillery *et al.* (1986b) observed the effect of stage of crop development on the diurnal fluctuation of pH in floodwater. According to them, the diurnal fluctuations in floodwater pH were lower when urea was added 5–7 days before panicle initiation. This effect probably resulted from lower photosynthetic rates in the floodwater, since the crop canopy was appreciably more dense in the fertilized areas that had earlier received the urea 14 or 21 days after transplanting. Fillery *et al.* (1984) also detected low rates of NH<sub>3</sub> loss after urea was applied to flooded rice at the panicle initiation stage. According to them, aside from N uptake, it appeared that the rice crop shaded floodwater and thereby suppressed the increased pH attributed to photosynthetic activity in floodwater.

Ventura and Yoshida (1977) reported that NH<sub>3</sub> volatilization in flooded soil increased markedly with an increase in soil pH, which implies that soil pH has some effect on floodwater pH. MacRae and Ancajas (1970) reported the same. Vlek and Craswell (1979), however, showed that soil pH has little effect on the pH of floodwater and therefore on NH<sub>3</sub> volatilization.

### 3. Effect of Secondary Factors on Floodwater Temperature

The secondary factors that influence the temperature in floodwater have an influence on the overall NH<sub>3</sub> volatilization process. Temperature of

floodwater seems to be a function of solar radiation, windspeed, relative humidity, water depth, plant cover, and suspended materials in floodwater.

The solar energy is received by the waterbody in the form of short-wave radiation. A fraction of incoming solar energy is returned to space by reflection/scattering as short-wave radiation. The fraction that is returned from incoming solar radiation is known as albedo. It is interesting to note, the albedo of a natural water surface, about 6%, is the lowest of any natural surface (Hasse and Dobson, 1986). According to them, heat storage is quite different for water versus solid surfaces. In water, part of the solar energy may penetrate to several meters depth, although strong surface (0–10 cm) heat stratification usually occurs in flooded rice. In water, the turbulent motions may distribute the heat absorbed in the uppermost few centimeters throughout a deeper layer. Therefore, water surface temperatures respond only slowly compared to land surface temperatures. Leuning *et al.* (1984), however, found that thermal stratification in turbid floodwater significantly influenced rates of  $\text{NH}_3$  loss. This may be due to a reduction in incoming solar radiation caused by suspended materials in floodwater. This shows that solar radiation, water depth, and suspended materials influence the temperature of floodwater.

Atmospheric conditions, such as windspeed and relative humidity, influence the evaporation of water from a free water surface. Floodwater temperature decreased by 3°C to 15°C when airflow rate was increased from 5 to 20 L/min. Lowering of temperatures with increasing airflow rate was due to an acceleration in evaporative cooling (Katyal and Carter, 1989).

#### *4. Effect of Secondary Factors on Water Depth*

Water depth is usually a function of supply and crop management practice. In irrigated agriculture, the farmer has the ability to control the water depth according to crop cultural needs. However, in rainfed agriculture during the wet season, intensity and duration of rainfall partially determine the depth of floodwater. Therefore, the depth of water can or cannot be controlled depending on the season, site, and the crop situation.

#### *5. Effect of Secondary Factors on Windspeed*

When there is a crop canopy, the effect of wind on the water surface becomes minimized. Therefore, the structure of the crop canopy is an

important secondary factor that influences the effect of windspeed on the water surface. The crop canopy also exerts a strong influence on the photosynthetic rates of the aquatic biota, which limits their effects on the water chemistry. Low rates of NH<sub>3</sub> loss (10–15% of the N applied) were detected after urea was applied in flooded rice at panicle initiation (Fillery *et al.*, 1984) and they concluded that dense plant canopy at panicle initiation may have restricted air exchange at the floodwater interface to minimize NH<sub>3</sub> volatilization.

## V. METHODS OF MEASURING AMMONIA VOLATILIZATION

There are various methods available to measure NH<sub>3</sub> volatilization from flooded systems. These include: (1) the enclosure methods with or without air exchange; (2) micrometeorological techniques; and (3) labeled tracer techniques. The methodology used generally influences the conclusions of a study and each of these methods has its own advantages and disadvantages. There are several excellent reviews on the methodologies used in NH<sub>3</sub> volatilization measurements (Terman, 1979; Vlek and Craswell, 1981; Fenn and Hossner, 1985; Fillery and Vlek, 1986; Harper, 1988).

Enclosure methods are most commonly used in NH<sub>3</sub> volatilization measurements (Denmead, 1983). There are a variety of enclosure designs that are used to measure NH<sub>3</sub> losses (Harper, 1988). These methods are simple and convenient, and can be used successfully to evaluate NH<sub>3</sub> losses under a variety of experimental variables. The disturbance of natural conditions, however, make the interpretations of these measurements somewhat questionable in terms of actual field conditions.

Micrometeorological techniques, on the other hand, have an advantage in that they do not disturb the natural environment conditions that influence NH<sub>3</sub> volatilization. They provide an average integrated flux over a large area, which minimizes the sampling variability. These techniques, however, are difficult to use in practice as they are costly in instrumentation, are laborious, and are site specific and weather dependent in their application to the experimental area. There are three general types of micrometeorological methods: (1) eddy correlation; (2) gradient diffusion; and (3) mass balance (Harper, 1988).

Labeled tracer N has also been used to calculate NH<sub>3</sub> loss. This is an indirect measurement and consequently, all other transformations including nitrification, denitrification, runoff, leaching, and plant uptake must be precisely determined to provide meaningful values for NH<sub>3</sub> volatilization. As stated by Harper (1988), <sup>15</sup>N balance cannot be used to evaluate NH<sub>3</sub>

loss from flooded soils since  $\text{NH}_3$  volatilization and nitrification-denitrification proceed simultaneously with the addition of N to the soil.

## VI. MODELS FOR PREDICTING AMMONIA VOLATILIZATION

Assessments of  $\text{NH}_3$  volatilization can be made by understanding the system represented by a simplified model. The behavior of  $\text{NH}_4^+\text{-N}$  in flooded soil systems and the mass transfer of  $\text{NH}_3$  across the water-air interface is a dynamic process, however, involving numerous interactions. In an  $\text{NH}_3$  volatilization model it is vital to understand the various chemical and physical processes controlling the emission rates. Few models have been developed to predict  $\text{NH}_3$  losses as a function of floodwater chemistry and atmospheric conditions (Bouwmeester and Vlek, 1981a; Moeller and Vlek, 1982; Jayaweera and Mikkelsen, 1990a).

### A. BASIC MODELS IN MASS TRANSFER

When there are two phases, the mass transfer of diffusing solute takes place from the bulk fluid of one phase into the interface, and then from interface to the bulk of the second phase. The concentration of the diffusing solute is virtually constant in the bulk fluid of both phases as a result of mixing caused by turbulence. Near the interface, in the boundary layer, the turbulence diminishes, resulting in a concentration gradient as the interface is approached and the mass flux experiences a resistance due to the mechanism of diffusion. Experimental verification of the conditions at or around the interface is difficult to achieve. Therefore, to understand the mass transfer in the interface region, it is necessary to develop theoretical models and validate these with overall mass-transfer experiments.

Few basic hydrodynamic models have been presented in the literature to describe mass transfer across a gas-liquid interface. All these models represent a simplified mode of mass transfer. The mass transfer between two phases is described by three major models: (1) film model; (2) penetration theory (Higbie's model); and (3) penetration theory (Danckwerts's model).

#### *1. Film Model*

The first hydrodynamic model to describe the transport processes between two phases was the two-film model by Whitman in 1923 (see Fig. 1).

He suggested that the resistance to transfer in each phase is confined in a thin stagnant, or laminar-flow film close to the interface between the two phases, in which the fluid is turbulent. This film is assumed to have a definite but unknown thickness. The mass transfer across these films is regarded as a steady-state process of molecular diffusion and it is assumed that there is no convection in the film.

### *2. Penetration Theory: Higbie's Model*

Higbie (1935) proposed a model to describe the hydrodynamic conditions in the liquid phase close to a gas-liquid interface. He suggested that the eddies in the fluid bring an element of fluid to the interface where it is exposed to the second phase for a definite interval of time, after which the surface element is mixed with the bulk again. Therefore, the fluid element where initial composition corresponds with that of the bulk fluid is remote from the interface, which is suddenly exposed to the second phase. This model considers the liquid surface to be composed of a large number of small elements that are being replaced by fresh elements from the bulk of the phase after a fixed time period. As the fresh liquid elements continually replace those interacting with the interface, the mass transfer is accomplished by the systematic removal of the interface.

The exposure time of such fluid elements at the interface is so short that steady-state conditions do not develop, and any mass transfer of material takes place only as a result of unsteady-state molecular diffusion.

### *3. Penetration Theory: Danckwerts's Model*

Danckwerts (1951) improved the surface renewal model proposed by Higbie, suggesting that the fluid element can have a variable surface residence time, which is exposed to the second phase; it may vary from zero to infinity. This means that each fluid element of surface would not be exposed for a constant time period as proposed by Higbie, but rather a random distribution of times could exist. This refinement of the surface renewal model is a result of an assumption that the probability of an element of surface being destroyed and mixed with the bulk fluid was independent of how long it has been on the surface.

All three models share the feature that the rate of mass transfer is directly proportional to the concentration difference. In many instances the difference between predictions made on the basis of these three models will be less than the uncertainties about the values of the physical quantities used in the calculations, and, therefore these models can be regarded

as interchangeable for many purposes. It is merely a question of convenience concerning which of the three models is used. When numerical computations are involved, it is generally simple to use Higbie's model rather than Danckwerts's model to compute the rate of transfer per unit area of the interface. The computations relating to the film model are, of course, simpler since they involve ordinary rather than partial differential equations. In most cases, however, the film model would lead to almost the same predictions as the surface renewal models (Danckwerts, 1970).

## B. BOUWMEESTER AND VLEK AMMONIA VOLATILIZATION MODEL

The  $\text{NH}_3$  volatilization model developed by Bouwmeester and Vlek (1981a) has a resemblance to the penetration theories of Higbie and Danckwerts. Major difference in their analysis, however, is that the surface liquid element has a known time of exposure to the atmosphere, depending on the wind velocity and the location of the element in the rice paddy.

By considering the following chemical reaction



where  $k_1$  and  $k_2$  are the forward and reverse rate constants, Bouwmeester and Vlek (1981a) developed the following relationship to calculate the average  $\text{NH}_3$  volatilization rate per unit area,  $\bar{Q}$ .

$$\bar{Q} = \frac{\bar{AN}}{\beta t_d} \left( \exp(\beta^2 D t_d) \operatorname{erfc} \beta \sqrt{D t_d} - 1 + \frac{2}{\sqrt{\pi}} \beta \sqrt{D t_d} \right) \quad (17)$$

where  $\bar{AN}$  is the ammoniacal N concentration in the bulk liquid; and  $t_d = F/U_d$  is the time during which the water chemistry, wind, and water conditions are supposed to remain steady depending on the fetch,  $F$ , and surface drift velocity,  $U_d$ ; and

$$\beta = k_a k_H / D(1 + R) \quad (18)$$

where  $k_a$  is the bulk transfer coefficient of  $\text{NH}_3$  in air,  $k_H$  is the Henry's constant, and  $D$  is the molecular diffusivities; and

$$R = (\text{H}^+ k_2 / k_1) = (\text{H}^+ / K) \quad (19)$$

where  $\text{H}^+$  is the hydrogen ion concentration in the system, and  $K$  is the equilibrium constant.

Equation (17) includes the effect of ammoniacal N concentration, pH,



temperature, wind, and fetch on the process of NH<sub>3</sub> volatilization. The temperature effects are reflected in the coefficients,  $D$ ,  $k_H$ , and  $R$ .

In developing the model, Boumeester and Vlek (1981a) assumed that for the time ( $t_d$ ) when the liquid element is at the surface, the chemical reaction does not change the pH. Hoover and Berkshire (1969) in studying the CO<sub>2</sub> exchange across an air–water interface also applied the same concept. They made this assumption because of the high mobility of the hydrogen ion. They argued that as the hydrogen ions have eight times the mobility of the bicarbonate ions, there would be no possibility of building up a significant concentration gradient. Therefore, the ratio NH<sub>3</sub>/NH<sub>4</sub><sup>+</sup> is constant throughout the diffusion layer with spectator ions maintaining the electroneutrality.

Bouwmeester and Vlek (1981a) validated the model in a wind–water tunnel experiment, which simulated the flooded rice paddies. Considering the complexity of the physical and chemical processes, they reported that the validation study seems to support the numerous assumptions made in developing the basic model equation in NH<sub>3</sub> volatilization. Although the quantitative agreement is not fully satisfactory, the results suggest that the mathematical model may be applied to analyze the rate-controlling factors of NH<sub>3</sub> volatilization from rice paddies.

By simulations they found that the rate of NH<sub>3</sub> volatilization is increased with increasing NH<sub>4</sub><sup>+</sup>-N concentration, pH, temperature, and wind velocity but is decreased with increasing fetch. The results suggest that the effects of wind, temperature, and pH on NH<sub>3</sub> volatilization are of the same order of magnitude. At a high pH, the volatilization rate of NH<sub>3</sub> is controlled by the transfer rate in the liquid diffusion layer and the effect of high windspeed is reduced. At low pH, the volatilization rate is limited mostly by the NH<sub>3</sub> transfer rate in the air.

### C. MOELLER AND VLEK AMMONIA VOLATILIZATION MODELS

Moeller and Vlek (1982) developed two mechanistic models, the pH constant model, and the pH gradient model, for the transport of NH<sub>3</sub> from aqueous solution to the atmosphere. These models are adaptations of the stagnant-film model used in studying gas exchange across an air–water interface (Danckwerts, 1970; Liss, 1973).

Considering Fick's first law of diffusion, and integrating over the thickness of the gas and liquid phase films, they obtained the following equations for the ammonia flux.

$$J_g = \frac{D_g}{\delta_g} ([\text{NH}_3]_g^a - [\text{NH}_3]_g^b) \quad (20)$$

where  $J_g$  is the  $\text{NH}_3$  flux in the gas phase,  $D_g$  is the diffusion coefficient of  $\text{NH}_3$  in air,  $\delta_g$  is the thickness of the gas film, and the superscripts b and o designate the bulk and surface concentrations or activities.

$$J_l = \frac{D_l}{\delta_l} (a_{\text{AN}}^b - a_{\text{AN}}^o) \quad (21)$$

where  $J_l$  is the total ammoniacal flux in the liquid phase,  $D_l$  is the diffusion coefficient for  $\text{NH}_4^+$  in aqueous solution,  $\delta_l$  is the thickness of the liquid film, and  $a_{\text{AN}}$  is the total ammoniacal activity

$$a_{\text{NH}_3} + a_{\text{NH}_4^+} = (1 + a_{\text{H}^+}/K_1) a_{\text{NH}_3} \quad (22)$$

where  $K_1$  is the equilibrium constant for  $\text{NH}_4^+/\text{NH}_3$  system.

At steady-state condition, when the diffusion flux through the liquid equals that through the gas, they obtained the following expression by equating the right-hand sides of Eqs. (20) and (21) and expressing the ammoniacal nitrogen activity at the surface in terms of  $\text{H}^+$ ,  $K_1$  and  $a_{\text{NH}_3}$ .

$$\frac{\delta_l D_g}{D_l \delta_g} ([\text{NH}_3]_g^o - [\text{NH}_3]_g^b) = a_{\text{AN}}^b - (1 + a_{\text{H}^+}/K_1) a_{\text{NH}_3}^o \quad (23)$$

The  $\delta_g$  and  $\delta_l$  parameters are determined experimentally. However, to solve for  $a_{\text{NH}_3}^o$  to calculate the flux using Eq. (21), it is necessary to determine three independent variables,  $[\text{NH}_3]_g^b$ ,  $a_{\text{H}^+}^o$ , and  $[\text{NH}_3]_g^o$ . Therefore, they obtained three additional relationships.

By assuming that the instantaneous steady-state flux is known, they obtained the following relationship to calculate  $[\text{NH}_3]_g^b$ .

$$[\text{NH}_3]_g^b = JA/S \quad (24)$$

where  $A$  is the surface area of the solution and  $S$  is the airflow rate being passed over the solution (volume/time). In practice, however,  $J$  is not known without having first solved for the surface concentrations. They used an iterative procedure with the bulk gas phase  $\text{NH}_3$  concentration set initially at zero and the surface concentration calculated in the manner described below. The  $\text{NH}_3$  flux can then be calculated and the bulk  $\text{NH}_3$  concentration can be determined.

By assuming that the aqueous  $\text{NH}_3$  and gas phase  $\text{NH}_3$  are in equilibrium at the interface, they obtained the following relationship for  $[\text{NH}_3]_g^o$ .

$$[\text{NH}_3]_g^o = k_H a_{\text{NH}_3}^o / (RT) \quad (25)$$

where  $k_H$ ,  $R$ , and  $T$  are the Henry's law constant for  $\text{NH}_3$ , the gas constant, and absolute temperature, respectively.

The surface hydrogen ion activity,  $a_{\text{H}^+}^o$  is determined by two different

methods, which differentiate the two models they developed. In the pH constant model, as assumed by Hoover and Berkshire (1969), they treated pH as a constant across the liquid film. Therefore,

$$a_{\text{H}^+}^{\text{o}} = a_{\text{H}^+}^{\text{b}}. \quad (26)$$

In the pH gradient model, by following the treatment of Quinn and Otto (1971), they developed a cubic expression for the surface hydrogen ion activity.

$$a_{\text{H}^+}^{\text{o}3} + p a_{\text{H}^+}^{\text{o}2} + q a_{\text{H}^+}^{\text{o}} + r = 0 \quad (27)$$

with

$$\begin{aligned} p &= a_{\text{AN}}^{\text{b}} + \frac{D_{\text{g}} \delta_{\text{l}}}{D_{\text{l}} \delta_{\text{g}}} [\text{NH}_3]_{\text{g}}^{\text{b}} + C K_{\text{l}} - 2\gamma[\text{SO}_4^{2-}] + \gamma[\text{Na}^+] \\ q &= -C K_{\text{l}} (2\gamma[\text{SO}_4^{2-}]) - \gamma[\text{Na}^+] - K_{\text{w}} \\ r &= -C K_{\text{l}} K_{\text{w}} \end{aligned} \quad (28)$$

and

$$C = \frac{\delta_{\text{l}} D_{\text{g}} K_{\text{w}}}{\delta_{\text{g}} D_{\text{l}} RT} + 1 \quad (29)$$

where  $\gamma$  is the activity coefficient,  $[\text{Na}^+]$  and  $[\text{SO}_4^{2-}]$  are the spectator ion concentrations, and  $K_{\text{w}}$  is the equilibrium constant for water.

Moeller and Vlek (1982) tested the two stagnant-film volatilization models in a series of laboratory experiments. They employed a small volatilization chamber connected to an airflow system, an experimental technique that is suited for the investigations of the fundamental processes of NH<sub>3</sub> volatilization in systems artificially maintained free of CO<sub>2</sub>.

It was evident from the experimental results that the model that assumes a pH gradient in the liquid diffusion film accurately predicts the observed volatilization rate, whereas the pH constant model does not. This indicates that the surface layer retains some importance as a resistance to volatilization at moderate and low pH. Bicarbonate and other buffers, however, can mitigate this pH gradient (Moeller and Vlek, 1982).

It is interesting to note that the effective thicknesses of the liquid- and gas-phase stagnant films calculated from NH<sub>3</sub> volatilization and water evaporation rates in the chamber are similar to corresponding parameters found in larger scale wind tunnel experiments. Therefore, Moeller and Vlek (1982) stated that it is possible to perform NH<sub>3</sub> volatilization studies in small chambers. Bouwmeester and Vlek (1981a,b) also reached a similar conclusion in their studies.

## D. JAYAWEERA AND MIKKELSEN AMMONIA VOLATILIZATION MODEL

The  $\text{NH}_3$  volatilization model developed by Jayaweera and Mikkelsen (1990a) computes the rate of  $\text{NH}_3$  volatilization as a function of five primary factors, which include the floodwater  $\text{NH}_4^+\text{-N}$  concentration, pH, temperature, depth of floodwater, and windspeed. In previous models researchers have taken these factors into consideration but not the depth of floodwater. The role of depth of floodwater in  $\text{NH}_3$  volatilization is twofold. It directly affects  $\text{NH}_4^+\text{-N}$  concentration by virtue of its dilution effect. Further, it influences the volatilization relationships (Jayaweera and Mikkelsen, 1990a).

## 1. Model Development

The ammonia volatilization model presented by Jayaweera and Mikkelsen (1990a) consists of two parts: (1) chemical aspects ( $\text{NH}_4^+/\text{NH}_{3(\text{aq})}$  equilibrium in floodwater); and (2) volatilization aspects ( $\text{NH}_3$  transfer from floodwater across the water-air interface).

*a. Chemical Aspects of the Model.* The chemical dynamics of  $\text{NH}_3$  volatilization from floodwater is described as follows:



where  $k_d$  and  $k_a$  are dissociation and association rate constants for  $\text{NH}_4^+/\text{NH}_{3(\text{aq})}$  equilibrium and  $k_{vN}$  is the first-order volatilization rate constant for  $\text{NH}_3$ .

By chemical kinetics, Jayaweera and Mikkelsen (1990a) derived the following expression to determine the rate of  $\text{NH}_3$  volatilization from a flooded system.

$$\frac{d[\text{NH}_4^+]}{dt} = k_a \left\{ \frac{k_d (AN - [\text{NH}_3]_{\text{aq}})}{k_a [\text{H}^+] + k_{vN}} \right\} - k_d (AN - [\text{NH}_3]_{\text{aq}}) \quad (31)$$

where  $AN$  is the ammoniacal N concentration,  $[\text{NH}_3]_{\text{aq}}$  is the aqueous  $\text{NH}_3$  concentration, and  $[\text{H}^+]$  is the hydrogen ion concentration in floodwater at equilibrium.

They have estimated the rate of  $\text{NH}_3$  volatilization by the rate of change in  $\text{NH}_4^+$  concentration in floodwater with the assumption that no other process changes the  $\text{NH}_4^+$  in the system. There are various processes, however, which bring  $\text{NH}_4^+$  into floodwater, such as soil desorption, organic matter mineralization, and those which remove  $\text{NH}_4^+$  from flood-

water, such as soil adsorption and biotic assimilation. It is assumed that these processes quickly equilibrate and subsequently affect little change in floodwater NH<sub>4</sub><sup>+</sup> concentration. Further, by making frequent NH<sub>4</sub><sup>+</sup> measurements and by using these values as model inputs, any error due to this assumption will be minimized.

Equation (31) estimates the rate of NH<sub>3</sub> volatilization as a function of ammoniacal N concentration, aqueous NH<sub>3</sub> and H<sup>+</sup> concentration in floodwater, rate constants  $k_d$  and  $k_a$  for the NH<sub>4</sub><sup>+</sup>/NH<sub>3(aq)</sub> equilibrium, and the volatilization rate constant for NH<sub>3</sub>,  $k_{vN}$ .

The NH<sub>4</sub><sup>+</sup>-N concentration and pH of floodwater are experimentally determined. Rate constants  $k_d$  and  $k_a$ , whose determination is discussed next, are computed in the chemical aspects of the model. Volatilization rate constant,  $k_{vN}$  is computed in the volatilization aspect of the model. Aqueous NH<sub>3</sub> is computed as a function of NH<sub>4</sub><sup>+</sup> concentration, pH, and temperature. The rate of NH<sub>3</sub> volatilization can be computed by applying these values to Eq. (31).

The rate constants at various temperatures are calculated in the model. First, the equilibrium constant,  $K$ , for the NH<sub>4</sub><sup>+</sup>/NH<sub>3(aq)</sub> system is computed, followed by the association rate constant,  $k_a$ . Finally, the dissociation rate constant,  $k_d$  is obtained with the use of  $K$  and  $k_a$ .

By applying the Clausius–Clapeyron equation to the NH<sub>4</sub><sup>+</sup>/NH<sub>3(aq)</sub> equilibrium, and by using the values  $pK$  at 25°C as 9.24 and  $\Delta H^\circ$  as 12,480 cal (Dean, 1986) Jayaweera and Mikkelsen (1990a) derived the following expression to compute  $pK$  at any temperature.

$$pK(T) = 0.0897 + \frac{2729}{T} \quad (32)$$

where  $pK(T)$  is  $-\log K$ , equilibrium constant for NH<sub>4</sub><sup>+</sup>/NH<sub>3(aq)</sub> system at absolute Kelvin temperature  $T$ . A similar equation has been derived by Bates and Pinching (1949) by a different methodology.

The association reaction between NH<sub>3</sub> and H<sup>+</sup> in water, as measured by Eigen and co-workers, is diffusion controlled (Alberty, 1983). Therefore, Jayaweera and Mikkelsen (1990a) assumed that the rate constant for the association reaction is proportional to the diffusion coefficient. By using Stokes–Einstein equation (Laidler and Meiser, 1982) and with the use of the association rate constant at 25°C (Alberty, 1983) and the viscosity of water at different temperatures (Dean, 1986), Jayaweera and Mikkelsen (1990a) developed the following relationship to compute  $k_a$  values as a function of absolute Kelvin temperature  $T$ .

$$k_a(T) = 3.8 \times 10^{11} - 3.4 \times 10^9 T + 7509700 T^2 \quad (33)$$

By using the equilibrium relationship, the dissociation rate constant,  $k_d$  for the NH<sub>4</sub><sup>+</sup>/NH<sub>3(aq)</sub> system at various temperatures can be computed.

$$k_d(T) = K(T) \times k_a(T) \quad (34)$$

where  $K(T)$  is the antilog of  $pK(T)$  at absolute Kelvin temperature  $T$ .

*b. Volatilization Aspects of the Model.* The volatilization aspect of the model is based on the two-film theory proposed by Whitman in 1923 and is used to compute the volatilization rate constant for  $\text{NH}_3$ ,  $k_{vN}$ . The controlling factor for the mass transfer of  $\text{NH}_3$  across the interface is the rate of diffusion through the two films on either side of the interface, where all the resistance lies. This shows the liquid phase or gas phase resistance or both, and determines the overall mass transfer rate of  $\text{NH}_3$ .

In developing this model, Jayaweera and Mikkelsen (1990a) have assumed that an  $\text{NH}_4^+/\text{NH}_{3(\text{aq})}$  equilibrium is established in the floodwater, and that  $\text{NH}_3$  in aqueous phase diffuses from the bulk of the liquid phase to the interface across the thin film. It is assumed, although perhaps inconclusively, that the pH in the surface film remains constant. Hoover and Berkshire (1969) and Bouwmeester and Vlek (1981a) made the same assumption in their gas exchange studies. Computation of various parameters of the volatilization aspects of the model is presented as follows:

1. Determination of volatilization rate constant for  $\text{NH}_3$ ,  $k_{vN}$ : By material balance of the  $\text{NH}_3$  system, Jayaweera and Mikkelsen (1990a) showed that the volatilization rate constant for  $\text{NH}_3$ ,  $k_{vN}$  is represented as a ratio:

$$k_{vN} = \frac{K_{ON}}{d} \quad (35)$$

where  $K_{ON}$  is the overall mass transfer coefficient for  $\text{NH}_3$ , and  $d$  is the mean depth of floodwater.

The relationship expressed by Eq. (35) shows that the volatilization rate constant for  $\text{NH}_3$  is inversely related to the depth of floodwater. To estimate the volatilization rate constant, however, it is necessary to know the overall mass transfer coefficient for  $\text{NH}_3$ ,  $K_{ON}$ .

2. Determination of overall mass transfer coefficient for  $\text{NH}_3$ ,  $K_{ON}$ : The rate of  $\text{NH}_3$  transfer through the gas film is the same as through a liquid film, under steady-state conditions. Since the movement through the film layers is by molecular diffusion, it can be described by Fick's first law of diffusion.

$$F_N = -D_N \frac{dC_N}{dx} \quad (36)$$

where  $F_N$  is the flux of  $\text{NH}_3$  gas through the surface films in  $x$  direction,  $D_N$  is the molecular diffusion coefficient or diffusivity of  $\text{NH}_3$ , and  $dC_N/dx$  is the concentration gradient of  $\text{NH}_3$  gas across the film of thickness  $x$ .

The ratio of  $D_N/\Delta x$  in Eq. (36) can be considered as a constant,  $k_N$ , under a given set of conditions and is the exchange constant for NH<sub>3</sub> gas, which has the dimensions of velocity,  $L/t$ .

$$k_N = - \frac{D_N}{\Delta x} \quad (37)$$

It is possible to obtain another form of the Fick's law equation generally used in gas exchange studies by substituting Eq. (37) into Eq. (36).

$$F_N = k_N \Delta C_N \quad (38)$$

where  $\Delta C_N$  is the concentration difference of NH<sub>3</sub> across the layer of thickness  $x$ .

By transforming Eq. (38), the exchange constant for NH<sub>3</sub>,  $k_N$ , is obtained as

$$k_N = \frac{F_N}{\Delta C_N} \quad (39)$$

Therefore, it is seen that the exchange constant for NH<sub>3</sub>,  $k_N$ , is a measure of the flux of NH<sub>3</sub> per unit concentration difference across the layer of thickness  $x$ . The value of  $k_N$  depends on many factors, of which the degree of turbulence in the fluids on both sides of the interface is important.

Under steady-state conditions and by applying Eq. (38) to the two-film situation and with the nondimensional form of Henry's law constant, Jayaweera and Mikkelsen (1990a) obtained the following expression after simplifying by introducing two constants:

$$F_N = K_{GN} (C_{gN} - H_{nN} C_{lN}) = K_{LN} [(C_{gN}/H_{nN}) - C_{lN}] \quad (40)$$

where

$$1/K_{GN} = 1/k_{gN} + H_{nN}/k_{lN} \quad (41)$$

and

$$1/K_{LN} = 1/k_{lN} + 1/H_{nN} k_{gN} \quad (42)$$

where  $K_{GN}$  and  $K_{LN}$  are the overall gas phase and liquid phase coefficients for NH<sub>3</sub>,  $k_{gN}$  and  $k_{lN}$  are the exchange constants for NH<sub>3</sub> in gas phase and liquid phase, respectively, and  $H_{nN}$  is the nondimensional Henry's law constant for NH<sub>3</sub>.

The total resistance of NH<sub>3</sub> transfer can be expressed on either a gas phase,  $1/K_{GN}$ , or a liquid phase,  $1/K_{LN}$ , basis. For convenience, Jayaweera and Mikkelsen (1990a) considered  $1/K_{LN}$  as the total resistance for NH<sub>3</sub> flux from a water body, and it was rearranged to determine the overall

mass transfer coefficient for  $\text{NH}_3$ ,  $K_{\text{ON}}$ , which is numerically equal to the overall liquid phase coefficient for  $\text{NH}_3$ ,  $K_{\text{LN}}$ .

$$K_{\text{ON}} = K_{\text{LN}} = (H_{\text{NN}} k_{\text{gN}} k_{\text{IN}}) / (H_{\text{NN}} + k_{\text{gN}} + k_{\text{IN}}) \quad (43)$$

To estimate  $K_{\text{ON}}$ , it is necessary to determine the nondimensional Henry's law constant for  $\text{NH}_3$ ,  $H_{\text{NN}}$ , and the gas and liquid phase exchange constants for  $\text{NH}_3$ ,  $k_{\text{gN}}$  and  $k_{\text{IN}}$ , respectively.

3. Determination of Henry's law constant for  $\text{NH}_3$ ,  $H_{\text{N}}$ ,  $\text{MPa m}^3/\text{mol}$ : Henry's law constant is a coefficient which represents the equilibrium distribution of a material between gas and liquid phases. The Henry's law constant should be obeyed reasonably well under flooded conditions, because of relatively low concentrations of  $\text{NH}_3$  in floodwater. Several researchers have used the Henry's law relationship in their  $\text{NH}_3$  volatilization studies in floodwater systems (Bouwmeester and Vlek, 1981a; Moeller and Vlek, 1982; Leuning *et al.*, 1984; Jayaweera and Mikkelsen, 1990a,b).

The Henry's law constant for  $\text{NH}_3$ ,  $H_{\text{N}}$ , in  $\text{MPa m}^3/\text{mol}$ , can be expressed in an equation form as follows:

$$H_{\text{N}} = \frac{P_{\text{N}}}{C_{\text{N}}} \text{MPa m}^3/\text{mol} \quad (44)$$

where  $P_{\text{N}}$  is the partial pressure of  $\text{NH}_3$  gas in MPa and  $C_{\text{N}}$  is the concentration of  $\text{NH}_{3(\text{aq})}$  in floodwater in  $\text{mol/m}^3$ .

a. Determination of partial pressure of  $\text{NH}_3$  gas,  $P_{\text{N}}$ , MPa: Jayaweera and Mikkelsen (1990a) derived an expression to estimate the mole fraction of  $\text{NH}_3$  in floodwater,  $X_{\text{N}}$ , as a function of pH and absolute temperature.

$$X_{\text{N}} = \frac{(C/17.03) (A/1 + A)}{(C/17.03) (A/1 + A) + (C/18.04) (1/1 + A) + 10^6 p_{\text{w}}/18.02} \quad (45)$$

where

$$A = 10 \exp (\text{pH} - 0.0897 - 2729/T) \quad (46)$$

$C$  is the total  $\text{NH}_4^+\text{-N}$  concentration in floodwater,  $\rho_{\text{w}}$  is the density of water in  $\text{gm/cm}^3$  at  $T$ , pH is the pH of floodwater, and  $T$  is the absolute Kelvin temperature of floodwater.

By using the Henry's law relationship, they obtained the following expression for the partial pressure of  $\text{NH}_3$  in the gas phase in equilibrium with its solution.

$$P_{\text{N}} = 18.62 \exp (-1229/T) X_{\text{N}} \text{MPa} \quad (47)$$

According to Eq. (45), the partial pressure of  $\text{NH}_3$  in the gas phase varies with  $\text{NH}_4^+\text{-N}$  concentration, pH, and temperature of floodwater.

b. Determination of concentration of  $\text{NH}_{3(\text{aq})}$ ,  $C_{\text{N}}$ ,  $\text{mol/m}^3$ : If the total ammoniacal N concentration is  $C$   $\text{mg/L}$ , by proper conversion, the con-



centration of NH<sub>3</sub>,  $C_N$ , can be determined in mol/m<sup>3</sup> (Jayaweera and Mikkelsen, 1990a).

$$C_N = (C/17.03) \frac{[10 \exp (\text{pH} - 0.0897 - 2729/T)]}{[1 + 10 \exp (\text{pH} - 0.0897 - 2729/T)]} \text{ mol/m}^3 \quad (48)$$

By using Eqs. (47) and (48), they obtained the Henry's law constant in MPa m<sup>3</sup>/mol.

4. Determination of nondimensional Henry's law constant for NH<sub>3</sub>,  $H_{nN}$ : Henry's law constant for NH<sub>3</sub>, which is computed in MPa m<sup>3</sup>/mol,  $H_N$ , can be transformed into nondimensional form as follows:

$$H_{nN} = \frac{H_N}{RT} \quad (49)$$

where  $R$  is the gas constant,  $8.315 \times 10^{-6}$  MPa m<sup>3</sup>/mol/deg K, and  $T$  is absolute Kelvin temperature.

5. Determination of gas phase,  $k_{gN}$ , and liquid phase,  $k_{lN}$ , exchange constants: Exchange constants have dimensions of velocity and can be considered as the velocity at which NH<sub>3</sub> moves through the fluid films. The value of exchange constants  $k_{gN}$  and  $k_{lN}$  depend on the degree of turbulence in the fluids on either side of the interface, chemical reactivity of the substance, temperature, and the properties of the solute, such as diffusivity or molecular size (Liss and Slater, 1974; Mackay and Yeun, 1983). These exchange constants, however, have not yet been readily computed using basic physical principles and generally are determined empirically (Thomas, 1982).

Henry's law constant of a chemical gives some insight into the distribution of resistances in the liquid and gas films. The Henry's law constant for NH<sub>3</sub> varies between  $4.36 \times 10^{-6}$  to  $6.59 \times 10^{-6}$  MPa m<sup>3</sup> mol in the usual temperature range found in floodwater, i.e., 10–40°C (Jayaweera and Mikkelsen, 1990a). According to the model developed by Jayaweera and Mikkelsen (1990a), the process of NH<sub>3</sub> volatilization is therefore controlled by both gas and liquid phase resistances (Mackay *et al.*, 1979). Liss and Slater (1974), however, suggested that the rate of NH<sub>3</sub> volatilization is controlled by the gas phase resistance, whereas Leuning *et al.* (1984) found that NH<sub>3</sub> fluxes were controlled by transport processes in both the atmosphere and the water.

By using the data of an experiment performed by Liss (1973) in a wind tunnel, a regression equation was developed to relate the water vapor exchange constant,  $k_{gw}$  (cm/h) and the windspeed (Jayaweera and Mikkelsen, 1990a).

$$k_{gw} = 18.5683 + 1135.89 U_{0.1} \quad (50)$$

where  $U_{0.1}$  is the windspeed at 0.1 m above the water surface in the wind tunnel.

Jayaweera and Mikkelsen (1990a) developed a relationship between the windspeed in the wind tunnel used by Liss (1973) and the equivalent field wind speed at 8 m:

$$U_8 = 1.5686 U_{0.1} \quad (51)$$

This is in close agreement with the relationship developed by Bouwmeester and Vlek (1981a).

The water vapor exchange constant,  $k_{gW}$  is transformed into field situations with Eq. (51), and is adjusted to  $\text{NH}_3$  transfer with the use of the molecular weight ratio of water and  $\text{NH}_3$  (Liss and Slater, 1974) to obtain the gas phase exchange constant for  $\text{NH}_3$ ,  $k_{gN}$  (Jayaweera and Mikkelsen, 1990a).

$$k_{gN} = 19.0895 + 742.3016 U_8 \quad (52)$$

Similarly, the  $\text{CO}_2$  exchange constant data of Liss (1973) were fit into a logistic equation and adjusted to field situation by Eq. (51) for the molecular weight ratios to obtain the liquid phase exchange constant for  $\text{NH}_3$ ,  $k_{iN}$ .

$$k_{iN} = \{12.5853/[1 + 43.0565 \exp(-0.4417 U_8)]\}1.6075 \quad (53)$$

By using the model (Jayaweera and Mikkelsen, 1990a),  $k_{iN}$  and  $k_{gN}$  values are computed at various windspeeds; both constants show an increase with increase in windspeed.

They have developed a relationship to transform the measured windspeed at any height over a water surface to a windspeed at 8 m height by assuming a logarithmic wind profile, which is used in the  $\text{NH}_3$  volatilization model (Jayaweera and Mikkelsen, 1990a).

$$U_8 = \frac{11.51}{\ln(Z/8 \times 10^{-5})} U_Z \quad (54)$$

where  $U_8$  is the windspeed at 8 m height in m/s, and  $U_Z$  is the windspeed at  $Z$  m height in m/s.

It should be noted, however, that Eq. (54) is based on the assumptions of neutral stability and windspeed measurements over flat water surfaces. These assumptions may be violated at night or at times of very low or very high evapotranspiration rates, or if plant cover exists above the water surface, which would decrease the accuracy of the equation (Jayaweera *et al.*, 1990).

## 2. Model Execution

The ammonia volatilization model (Jayaweera and Mikkelsen, 1990a) is executed with several input variables. They are floodwater NH<sub>4</sub><sup>+</sup>-N concentration, mg/L (AMC); pH; temperature, °C (TEMP); depth of floodwater, cm (WD); windspeed, m/s (WS); and the height of wind measurement, m (WH) (Fig. 11). The model calculates the initial volatilization rate of NH<sub>3</sub> (VRAMI). Ammonia loss for a specific period is obtained by entering the time period as an input and the model computes the decrease in volatilization rate as a function of the time with a successive approximation loop. The final output is the predicted NH<sub>3</sub> loss for the selected time period.

## 3. Sensitivity Analysis

The sensitivity analysis has been performed on the model to test the influence of various determinants on NH<sub>3</sub> volatilization. Floodwater NH<sub>4</sub><sup>+</sup>-N concentration shows a linear relationship to NH<sub>3</sub> volatilization when other factors such as pH, temperature, depth of floodwater, and windspeed are kept constant. This direct relationship is due to an increase in NH<sub>3(aq)</sub> in floodwater as a function of NH<sub>4</sub><sup>+</sup>-N concentration as has been reported (Vlek and Stumpe, 1978; Vlek and Creswell, 1979; Fillery and Vlek, 1986; Jayaweera and Mikkelsen, 1990b). Therefore, in the sensitivity analysis performed by Jayaweera and Mikkelsen (1990b), the floodwater NH<sub>4</sub><sup>+</sup>-N concentration is kept at a constant value of 25 mg/L.

The effect of four other factors, pH, temperature, depth of floodwater, and windspeed were tested in sensitivity analysis under these different sets of conditions. At each condition, one factor is varied while the others are kept constant. The final output, NH<sub>3</sub> loss per day, is shown in Fig. 12.

The sensitivity (slope) of NH<sub>3</sub> loss per day with respect to pH, temperature, water depth, and windspeed is shown in Table I. A detailed account of the sensitivity analysis was presented by Jayaweera and Mikkelsen (1990b).

In summary, under conditions 1, 2, and 3, pH was the most sensitive variable; temperature was the least sensitive under conditions 1 and 2; and water depth showed the least sensitivity under condition 3 (Table I, Fig. 12).

The sensitivity analysis shows clearly that it is not possible to generalize on the effect of one variable without considering the other interacting conditions. Therefore, the magnitude of NH<sub>3</sub> loss from floodwater can be predicted only by taking into account all five primary factors simulta-

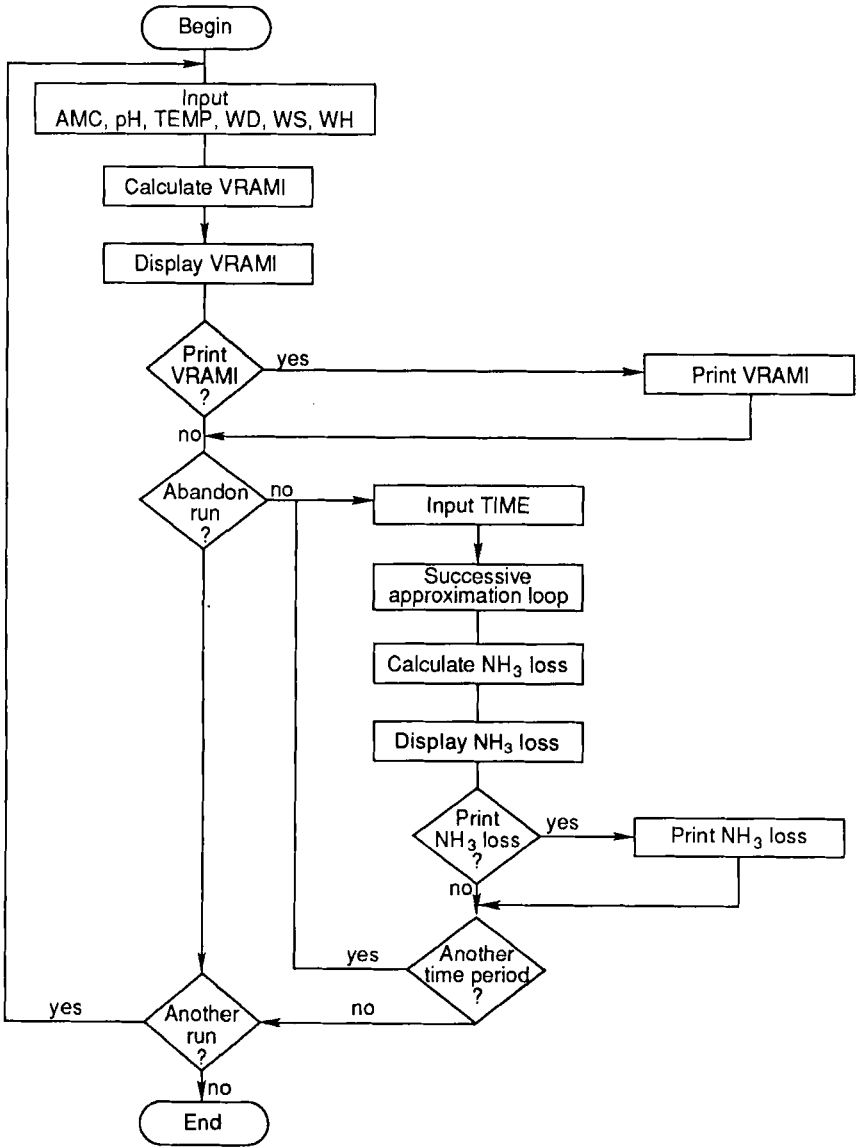
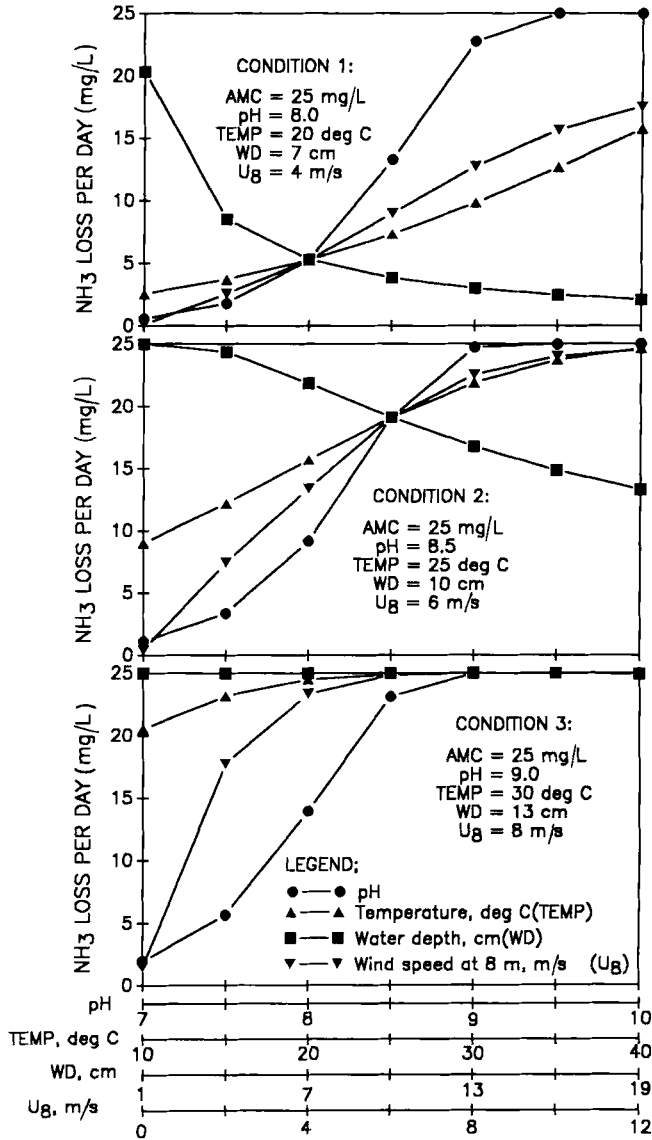


FIG. 11. Flow chart for  $\text{NH}_3$  volatilization model. (From Jayaweera and Mikkelsen, 1990b.)



**FIG. 12.** Sensitivity analysis for NH<sub>3</sub> volatilization model AMC (NH<sub>4</sub><sup>+</sup>-N concentration in floodwater). (From Jayaweera and Mikkelsen, 1990b.)

**Table I**  
**Sensitivity Analysis of Model (Slope) Affected by pH, Temperature, Depth of Floodwater, and Windspeed<sup>a</sup>**

Condition	Percent NH <sub>3</sub> loss/d/unit change					
	pH <sup>c, d, e</sup>					
	7.25	7.75	8.25	8.75	9.25	9.75
1	2.5	7.0	16.0	19.0	4.5	0.0
2	4.5	11.6	20.0	11.3	0.5	0.0
3	7.4	16.5	18.4	3.7	0.0	0.0
	Temperature, °C <sup>b, d, e</sup>					
	12.5	17.5	22.5	27.5	32.5	37.5
1	0.2	0.3	0.4	0.5	0.6	0.6
2	0.6	0.7	0.7	0.6	0.4	0.2
3	0.5	0.3	0.9	0.0	0.0	0.0
	Water depth, cm <sup>b, c, e</sup>					
	2.5	5.5	8.5	11.5	14.5	17.5
1	-3.9	-1.1	-0.5	-0.3	-0.2	-0.1
2	-0.2	-1.0	-0.9	-0.8	-0.6	-0.5
3	0.0	0.0	0.0	0.0	0.0	0.0
	Windspeed, m/s <sup>b, c, d</sup>					
	1	3	5	7	9	11
1	1.2	1.4	1.9	1.5	1.5	0.9
2	3.5	3.0	2.7	1.7	0.7	0.3
3	8.1	2.8	0.8	0.0	0.0	0.0

<sup>a</sup> NH<sub>4</sub><sup>+</sup>-N concentration was 25 mg/L for all three conditions.

<sup>b</sup> pH values for conditions 1, 2, and 3 were 8.0, 8.5, and 9.0, respectively.

<sup>c</sup> Temperatures for conditions 1, 2, and 3 were 20, 25, and 30, respectively.

<sup>d</sup> Water depths for conditions 1, 2, and 3 were 7, 10, and 13, respectively.

<sup>e</sup> Windspeeds for conditions 1, 2, and 3 were 4, 6, and 8, respectively.

neously, which determine the NH<sub>3(aq)</sub> concentration and the volatilization rate constant for NH<sub>3</sub>.

#### 4. Model Validation

The ammonia volatilization model predicting NH<sub>3</sub> loss as a function of input variables was validated using a wind tunnel to simulate rice paddy conditions and direct field experiments (Fig. 13) (Jayaweera *et al.*, 1990).

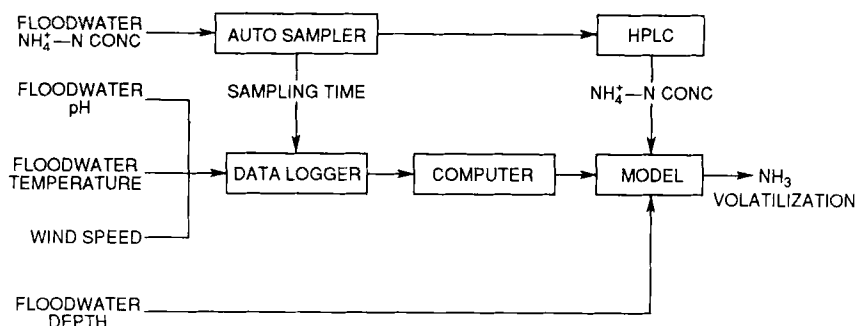


Fig. 13. Diagrammatic representation of the experimental field setup. (From Jayaweera *et al.*, 1990.)

There were a total of 13 wind tunnel runs to determine the effect of 5 composite combinations of variables on NH<sub>3</sub> volatilization. A central composite statistical design including mean values for each variable, as well as maximum and minimum values of each variable, were used in the experiment as described in Table II.

The solution samples collected during the wind tunnel runs show the NH<sub>4</sub><sup>+</sup>-N depletion rate under various treatment conditions. For each run, by using first-order kinetics, a straight line was fitted after logarithmic transformed concentration values and the rate constants and half-life values of NH<sub>4</sub><sup>+</sup>-N depletion were calculated. The highest rate constant and the shortest half-life for NH<sub>4</sub><sup>+</sup>-N depletion were observed when the pH is 10.5 and the lowest rate constant and the largest half-life value occurred when the pH is 6.5. It is interesting to note that the rate constant almost doubled, from 0.00028 to 0.00054, when the temperature was increased from 20 to 30°C, which is common for chemical reactions (Jayaweera *et al.*, 1990).

The average value for the predicted ÷ observed NH<sub>3</sub> loss for the 13 wind tunnel runs is 1.2, suggesting that on the average, the model predicted NH<sub>3</sub> loss quite close to the observed values under the experimental conditions in the wind tunnel. Linear regression of the observed NH<sub>3</sub> loss on predicted values indicates that the regression coefficient  $R^2$  improved greatly when the high windspeed (8.9 m/s), high pH (10.5), and low pH (6.5) runs were omitted, indicating that the model has some limitations under certain conditions. Then the regression equation becomes

$$\text{observed NH}_3 = -0.43 + 0.99 (\text{predicted NH}_3 \text{ loss}) \quad (55)$$

with a  $R^2$  of 0.98.

The close fit (Fig. 14) of the observed on predicted values shows that the

**Table II**

**Experimental Details, Equivalent Field Windspeed at 8 m Height,  $U_8$ , and Observed and Predicted  $\text{NH}_3$  Loss for Wind Tunnel Runs**

Variable (Wind tunnel run)	Initial $\text{NH}_4^+\text{-N}$ conc. (mg/L)	pH	Temp. (°C)	Water depth (cm)	Free stream windspeed (m/s)	$U_8$ (m/s)	Observed $\text{NH}_3$ loss (mg/L)	Predicted $\text{NH}_3$ loss (mg/L)	Predicted ÷ observed
Mean (1)	52.3	8.5	25	11.0	2.9	4.4	8.3	9.5	1.1
Mean (2)	52.6	8.5	25	11.0	2.8	4.2	8.3	9.1	1.1
Mean (3)	53.2	8.5	25	11.0	2.7	4.1	7.9	8.9	1.1
$\text{NH}_4^+\text{-N}$ concentration									
Low (4)	26.2	8.5	25	11.0	2.6	4.1	3.5	4.3	1.2
High (5)	102.5	8.5	25	11.0	2.7	4.1	24.8	49.8	2.0
pH									
Low (6)	52.7	6.5	25	11.0	2.6	4.1	1.8	0.1	0.1
High (7)	49.8	10.5	25	11.0	2.9	4.4	24.8	49.8	2.0
Temperature									
Low (8)	52.5	8.5	20	11.0	2.7	4.1	5.5	6.2	1.1
High (9)	53.1	8.5	30	11.0	2.9	4.4	11.8	13.3	1.1
Water depth									
Low (10)	52.7	8.5	25	6.4	2.8	4.2	14.6	14.6	1.0
High (11)	50.3	8.5	25	21.3	2.8	4.2	4.5	4.7	1.0
Windspeed at 8 m									
Low (12)	51.6	8.5	25	11.0	1.9	2.9	6.5	5.7	0.9
High (13)	52.9	8.5	25	11.0	5.3	8.2	12.2	22.3	1.8



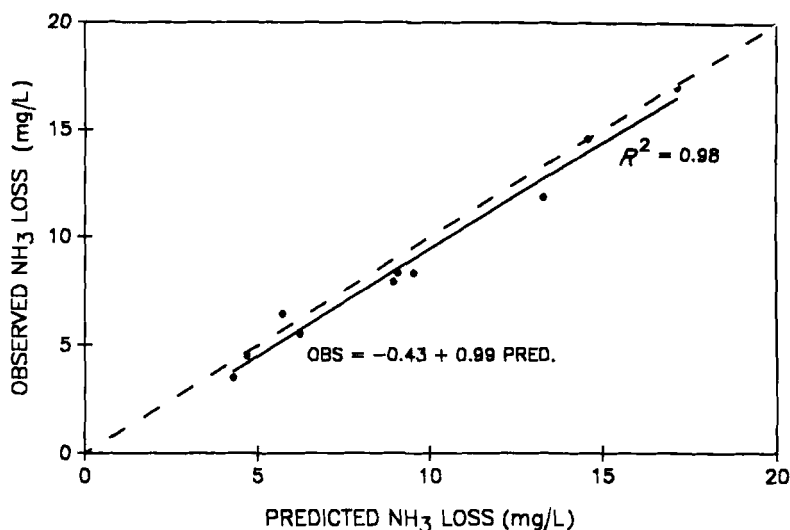


FIG. 14. Regression of observed on predicted NH<sub>3</sub> loss in wind tunnel runs. (From Jayaweera *et al.*, 1990.)

model predicted NH<sub>3</sub> loss quite well within the range of conditions usually found in flooded systems.

Field experiments show a close agreement of predicted values with observed data collected during 3 days at two different time periods and averaged for 6 h and 24 h (Fig. 15). Regression of observed NH<sub>4</sub><sup>+</sup>-N depletion data on predicted values to test the closeness of fit also showed a close agreement. However, as the averaging period is increased to 24 h, the regression slope is increased to a value slightly greater than 1.0, and the intercept decreases below 0 (Jayaweera *et al.*, 1990).

In general, it is seen that observed values from the wind tunnel and field experiments agreed closely with the predicted values from the model. By scrutinizing the data (Jayaweera *et al.*, 1990) it is established that the amount of NH<sub>3</sub> loss, which is a function of volatilization rate of NH<sub>3</sub>, is quantitatively described by the concentration of NH<sub>3(aq)</sub> in the floodwater, which in turn is governed by NH<sub>4</sub><sup>+</sup>-N concentration, pH and temperature of floodwater, and the volatilization rate constant for NH<sub>3</sub>,  $k_{vN}$ , which is a function of temperature, water depth, and windspeed.

The NH<sub>3</sub> volatilization model presented by Jayaweera and Mikkelsen (1990a,b) has several unique features. It has a menu-driven computer program that can be easily executed. It requires only 5 input variables to predict NH<sub>3</sub> loss and no input constants since the model computes all necessary constants, depending on the variables provided. Input variables

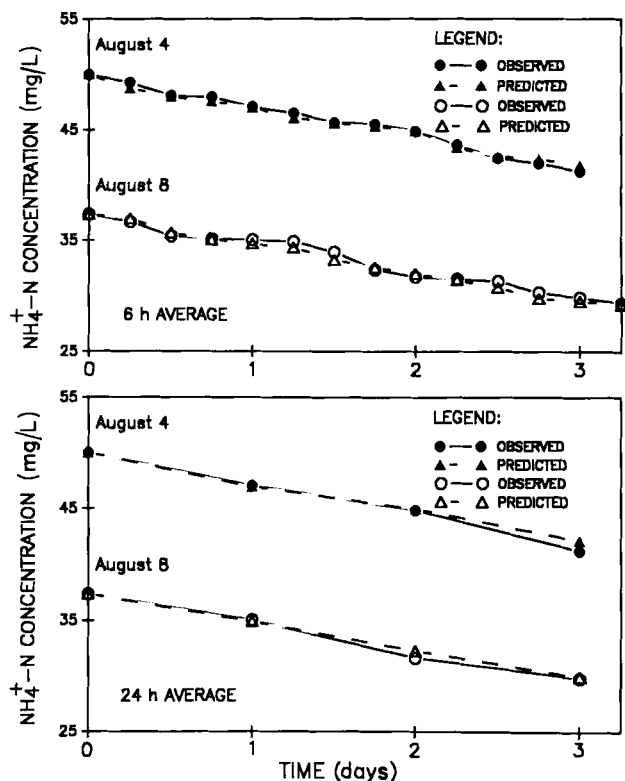


FIG. 15. Predicted and observed  $\text{NH}_4^+-\text{N}$  depletion in the field. (From Jayaweera *et al.*, 1990.)

are easily measurable with simple, inexpensive instrumentation. Analytical measurements are needed only for the initial foodwater  $\text{NH}_4^+-\text{N}$  concentration. Depth of floodwater is measured initially and generally remains constant, thus frequent measurements are needed for only three variables, pH, temperature, and windspeed (Jayaweera *et al.*, 1990).

Jayaweera *et al.* (1990) concluded that the model is useful in simplifying the complex  $\text{NH}_3$  volatilization process by considering only two major parameters: (1) aqueous  $\text{NH}_3$  concentration; and (2) volatilization rate constant for  $\text{NH}_3$  as a function of five variables,  $\text{NH}_4^+-\text{N}$  concentration, pH, temperature, water depth, and windspeed, which determine the volatilization rate of  $\text{NH}_3$  to accurately predict the  $\text{NH}_3$  loss in the range of conditions found in flooded systems.

## VII. EPILOGUE

Ammonia volatilization is a major mechanism for N loss from flooded soil systems such as rice paddies, ponds, lakes, wastewater ponds, and manufacturing systems. Losses of NH<sub>3</sub> from rice paddies have been identified as a factor associated with low fertilizer use efficiency and reduced crop yields.

The preceding discussion has been directed primarily to the basic aspects of NH<sub>3</sub> volatilization wherein NH<sub>4</sub><sup>+</sup>-N concentrations in floodwater directly influence aqueous NH<sub>3</sub> levels and where water pH and temperature determines the fraction of NH<sub>4</sub><sup>+</sup>/NH<sub>3</sub> dissociation. The higher the water NH<sub>4</sub><sup>+</sup>-N content and water pH and temperature, the higher is the aqueous NH<sub>3</sub> concentration and NH<sub>3</sub> volatilization from floodwater. It is shown that the volatilization rate constant for NH<sub>3</sub> is determined by temperature, water depth, and wind speed. Elevated water temperatures, high wind speeds, and shallow water depths increase the volatilization rate constants, and consequently the quantity of NH<sub>3</sub> to be lost from flooded soil systems.

Theoretical aspects of the models are presented together with laboratory and field verification data in such a manner that the NH<sub>3</sub> volatilization process can be understood and assessments can be made of NH<sub>3</sub> volatilization losses. Only two parameters, aqueous NH<sub>3</sub> concentration and the volatilization rate constant for NH<sub>3</sub> as influenced by 5 variables (water NH<sub>4</sub><sup>+</sup>-N concentration, pH, temperature, water depth, and wind speed), figure prominently in NH<sub>3</sub> volatilization process.

A knowledge of how NH<sub>3</sub> volatilization occurs, assessments of field losses in agricultural crop production, and an appreciation of how agronomic principles can be used will help to minimize losses. Improved crop, soil, and water management practices can be used to increase N-use efficiency (especially in flooded rice), to conserve costly fertilizer materials, and to minimize environmental pollution.

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